

**DRY ANAEROBIC DIGESTION OF
MUNICIPAL SOLID WASTE**

A Thesis

Presented to the Faculty of Graduate Studies
of the University of Manitoba
in Partial Fulfilment for the
Degree of Master of Science

by

Dennis Mark Heinrichs

August 1990



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DENNIS MARK HEINRICHS

A thesis submitted to the Faculty of Graduate Studies of
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ABSTRACT

Anaerobic digestion of municipal solid waste enriched with waste secondary sludge has been accomplished at solids concentrations of 20 to 40%. By utilizing the waste near its original solids level, handling and water requirements were minimized. Valuable end-products of methane and compost were obtained.

Experimental work involved the anaerobic digestion of a synthetic municipal solid waste (MSW), made using high newsprint content and food waste, supplemented with waste sewage sludge (WSS). The responses measured were biogas productivity, percent methane, total solids and volatile solids, alkalinity, pH, and volatile fatty acid concentration. This study was undertaken to determine the optimum temperature, solids level, and MSW:WSS ratio for a high paper content North American waste and to gain a further understanding of the effects of various operational variables.

Dry anaerobic digestion was successful at solids levels beyond 20%. Optimum biogas production rates were realized in thermophilic digesters. Mesophilic digesters with same operating parameters, were more stable in operation but yielded 30% less biogas. Optimum operating parameters found in this study were solids concentration of 30 to 35%, longer retention time of 21 days, and a MSW:WSS ratio of one.

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1.0 INTRODUCTION

Energy can be recovered from municipal solid waste (MSW) through either incineration or methane collection resulting from anaerobic decomposition (Chynoweth and Legrand, 1988). Generation of methane has been accelerated through leachate recycle in landfills (in-situ recovery) or through batch anaerobic digestion, at various total solids (TS) levels (Ten Brummeler et al., 1988; Kasali and Senior, 1989).

High solids anaerobic digestion has been achieved at total solids concentrations above 20%. Most municipal solid waste generated has a solids content near 40% TS (Ali Khan and Burney, 1989). By utilizing the waste near its original solids level, handling and water requirements are minimized. Dry anaerobic digestion (DAD) reduces volumes to be processed and may eliminate liquid effluent. DAD produces valuable end-products of methane and compost (Wujcik, 1980).

One of the demonstrated ways of increasing the rate of digestion has been co-digestion of MSW with waste secondary sludge (Six and DeBaere, 1988). Other methods investigated included increasing digestion temperature, lowering solids concentration, increasing nutrient supply as well as other process variations (Pfeffer, 1973; Cecchi et al., 1988; Graindorge et al., 1989).

The effects of variations in temperature, solids concentration, sludge content, along with other operational

variables such as waste composition have not been well documented. Several European continuous-feed high solids anaerobic digesters are at the pilot plant stage, with one on a commercial level. Little information on high solids anaerobic digestion has been gained from these plants due to their commercial nature.

The MSW found in North America has a much higher paper content in comparison to European urban waste (Graindorge et al., 1989). The MSW in this study was a synthetic waste, made up of newsprint and food waste, supplemented with waste secondary sludge (WSS).

The goal of this study was to determine the optimum operational parameters for a high newspaper content municipal solid waste supplemented with waste secondary sludge. Operational variables considered were:

- temperature
- solids concentration
- MSW:WSS ratio and
- mass retention time.

Performance indicators used were:

- biogas productivity
- biogas composition
- removal efficiency
- VFA concentration
- pH and
- alkalinity.

2.0 LITERATURE REVIEW

The following literature study is intended to cover the operational parameters important to the in-vessel anaerobic digestion of high solids, particularly as it relates to MSW and waste sludge degradation. Municipal solid waste composition and end-product use are presented. Anaerobic digestion in landfills and batch in-vessel digestion are also covered to a lesser degree. The discussion does not intend to describe anaerobic digestion in general. This topic has been well covered by many others (Parkin and Owen, 1986; Pfeffer, 1979). Table 1 gives a comparison of results from both continuous and batch studies.

2.1 Effect of Solids Concentration

The effect of solids concentration on substrate degradation has been reported to be significant. In sludge digestion, an increase in total solids decreases process efficiency. In high solids digestion of manure substrate mixtures, methane production decreased considerably between 30 and 35% TS (Wujcik and Jewell, 1988). Graindorge et al. (1989) digested MSW with high levels (40%) of paper and cardboard, they found that due to the rheology of the digestate a solids concentration of 25% should not be exceeded. Present Valorga operating solids level was reported to be 35% TS for a highly fermentable organic waste.

SUBSTRATE	Fermentable		Fermentable		North American		Dairy Manure	Wheat Straw, Dairy Manure and Water	compost/MSW 1/4, with seed sludge	30% cardboard 30% newsprint 20% magazine 10% kitchen paper 10% white paper
	Fermentable OMSW	Precomposted OMSW	OMSW & cardboard	MSW+WSS	MSW+WSS	MSW+WSS				
MRT, day	14	21	17	21	21	22	15	20	10	batch
TS feed %	34-40	32-36	30	35	35	20.4	20.4	25	25	35
Lignin, % of TS	N/A	N/A	10	17	17	15.5	15.5	N/A	N/A	5.6
Temp. C	35	35	40	39	53	35	35	35	35	30
Loading Rate kg VS/m ³ *d	12.9	11	6.6	4.82	4.9	7.5	11.6	7.86	15.7	batch
Removal Efficiency % VS basis	41	64	42	49.6	62	29.5	23.3	28.3	8.5	55
Biogas Productivity m ³ BG/m ³ wv*d	3.8	5.1	2.18	1.72	2.17	1.6	2.1	1.6	0.96	batch
Biogas Yield m ³ BG/kg VS rem.	N/A	N/A	0.786	0.72	0.72	0.70	0.73	0.72	0.72	0.78
Biogas Pseudo-Yield m ³ BG/kg VS fed	0.295	0.464	0.33	0.357	0.444	0.20	0.17	0.20	0.06	0.429
Reference	(DeBaere et al., 1985)	(Graindorge et al., 1989)	(Graindorge et al., 1989)	(Poggi-Viraldo et al., 1990; present work)	(Hills (1), 1980)	(Hills (1), 1980)	(Hujcik, 1980)	(Graindorge et al., 1989)	(Ten Brummeler et al., 1988)	

N/A - not available

- - estimated

Table 1: Comparison of Results of Various Anaerobic High Solids Studies

Researchers using the Dranco process have been operating at a total solids level of 30 to 35%, digesting a highly fermentable organic MSW (OMSW) (DeBaere et al., 1985). Research to date indicates that digestion of highly fermentable OMSW is most feasible in the range of 30 to 35% TS. Higher paper content wastes have not been examined in detail.

2.2 Effect of Temperature

In the batch digestion of OMSW, temperature was found "to exert significant effects on the interrelated metabolic processes of acidogenesis, solventogenesis, and methanogenesis" (Kasali and Senior, 1989). At 40% TS, thermophilic temperatures (55 °C) proved inhibitory to biogas production and there was an accumulation of solvents. A bactericidal effect was observed to occur on the methanogens at the 55 °C incubation temperature. It was concluded that optimal rates of methanogenesis can be maintained only at mesophilic temperatures.

Debaere et al. (1985) observed both mesophilic and thermophilic OMSW digesters, producing similarly $6.2 \text{ m}^3/\text{m}^3\text{r}\cdot\text{d}$ at loadings of 14.3 to 17.2 kg COD/ $\text{m}^3\cdot\text{d}$, using a highly fermentable OMSW. At a higher loading rate, of 18.6 kg COD/ $\text{m}^3\cdot\text{d}$ mesophilic gas production decreased by about 10%. With a higher COD loading of 21.4 kg/ $\text{m}^3\cdot\text{d}$ the thermophilic digestion rate increased to $8.5 \text{ m}^3 \text{ biogas}/\text{m}^3\text{r}\cdot\text{d}$. At the total solids content of 30 to 35%, the thermophilic digester was capable

of operating at a loading rate 25% above the maximum mesophilic loading rate.

Using landfilled MSW with 39 to 57% TS, optimum operating temperatures reported by other researchers have been 41 °C (Hartz et al., 1982) and 42 °C (Mata-Alvarez and Martinez-Virturtia, 1986 in Kasali and Senior, 1989).

At a long retention time of 30 days, Pfeffer (1973) found thermophilic digestion in slurries (4 to 10% TS) to be 60% more efficient than mesophilic. Using landfill slurries (greater than 5% TS), 50% greater gas production rates were reported for a 30 day retention time at thermophilic temperatures compared to mesophilic (Cooney and Wise, 1975 in Kasali and Senior, 1989). Using piggery and dairy wastes (3-18% TS), performance of thermophilic digesters was more efficient with increasing loading conditions. At a retention time of 6 days, 30% more gas production was realized at thermophilic than mesophilic temperatures (Kimchie et al., 1988).

Seemingly contradictory to the above findings, Buivid et al. (1981) demonstrated the importance of temperature and the initial methanogenic population by adding digested sewage sludge to refuse. In the presence of a 10% (w/w) inoculum, the total volume of the methane evolved was higher at 60 °C than 37 °C. When the inoculum was reduced to 5% (w/w), there were reductions in methanogenesis such that only 2% of the methane generated at 37 °C was produced at 60 °C.

Thermophilic operating temperatures appear to result in higher removals and efficiencies. Other researchers report operational difficulties in the thermophilic range. The effect of temperature, although present, is not definitive.

2.3 Effect of Retention Time/Loading Rate

In the digestion of barley straw and dairy manure at an average total solids of 13%, 35 °C, methane production was reported to be 1.27 to 2.46 m³/m³r*d, at loading rates of 5.2 to 12.5 kg VS/m³*d respectively. Efficiency was reported to be fairly constant for retention times (RT) greater than 20 days but dropped off considerably for retention times less than 15 days. With a decrease in retention time from 25 to 10 days the same researcher observed a decrease in methane content from 62.5% to 57.4% (Hills, 1980a).

Other researchers, using a 6% TS slurry of OMSW with primary sludge (PS) or WSS, found that the best results from an economical and processing point of view were obtained at a retention time of 14 to 15 days. Below this point there was a wash-out of bacteria. Beyond two weeks biogas remained relatively constant indicating 15 days as the most economical retention time (Cecchi et al., 1988).

In another study, an increase in retention time from 17 to 25 days did not significantly improve conversion of organic matter. An increase in conversion from 51% to 56% was

reported. For OMSW containing 42% paper and cardboard, a 17 d RT with 25% TS was recommended (Graindorge et al., 1989).

Using a systems analysis approach, Chynoweth and Legrand (1988) determined the optimum economical retention time for high solids anaerobic digestion to exist near 3 weeks. Researchers report that optimum MRT may vary from 15 to 25 days depending on temperature, solids concentration and substrate.

2.4 Effect of pH and VFA

Most researchers found that it was necessary to provide buffering to high solids digestion, suggesting higher rates in hydrolysis and acidogenesis. Methanogenic populations have been seen as the rate limiting step. Mao and Pohland (1973) found that in sludge-seeded studies, methanogenic bacteria were soon outnumbered by acidogenic species, due to their sensitivity to oxygen and their lower specific growth rates.

Calcium carbonate was not effective in buffering (Ten Brummeler et al., 1988). Jewell et al. (1981) found CaCO_3 did not control pH sufficiently. Sodium bicarbonate gave best results. The initial buffer/substrate solids ratio was 0.06. The actual Na^+ concentration during the study was 8.9 g/L, which exceeded reported toxicity levels for methanogens (Duarte and Anderson, 1982 in Ten Brummeler et al., 1988). In batch studies using hand-sorted landfill refuse at 40% TS, 2.5% (w/v), sodium bicarbonate was shown to promote fermenta-

tion. A lower concentration near 1% is speculated to be more cost effective in conjunction with the optimization of different variables such as refuse density, moisture content, pH or temperature (Kasali et al., 1989a).

DeBaere and his colleagues found volatile fatty acids were inhibitory to the hydrolysis phase at relatively low concentrations so that only a maximum of 20-30 g/L were produced in the form of volatile acids and lactic acid. The pH at this point was reported to be low, between 5.5 and 7.0. Above this concentration of organic acids, hydrolysis was reported to cease (DeBaere et al., 1985).

In the operation of dry anaerobic digesters buffering has been recommended to maintain pH near neutral. Volatile fatty acid concentration has shown to become inhibitory if allowed to accumulate.

2.5 Effect of Digestate Composition

The composition of urban municipal solid waste can greatly affect the performance of digestion. Table 2 gives a breakdown of the typical wastes from European and North American cities. Paper and cardboard make up 45% of Canadian urban waste. European urban waste contains a greater percentage of highly fermentable organics and less paper.

	(F)	EUROPE (FRG)	(UK)	NORTH AMERICA (U.S.A.) (CAN.)	
Paper and Cardboard	30	20	33.9	37.1	45
Biodegradable	25	42.3	23.4	26	26
Fines	17	11.5	7.1	--	1
Inerts (total)	19	23.1	25.7	28.4	20.4
Glass	8	11.6	14.4	9.7	6.5
Metals	6	3.9	7.1	9.6	6.4
Plastics	5	7.6	4.2	7.2	5.7
Miscellaneous	9	3.1	9.9	8.5	7.8

(per cent weight)

(Bonomo and Higginson, 1988)

Table 2: Urban Refuse Composition Data

The paper fraction of the OMSW has been shown to be the most difficult organic fraction in anaerobic degradation. Newsprint contains 80% machine produced pulp and paper and therefore has the highest lignin content of all cardboard and papers. Lignin is thought to be insoluble and non-biodegradable under anaerobic conditions. It has negative effects on degradation when combined with cellulose (Graindorge, 1989). Ligneous structure within an organic complex tends to shield the cellulose materials from enzymatic hydrolysis (Hills, 1980b).

As already mentioned earlier, the seeding with sewage sludge has been shown to enhance the performance of a high solids process. DeBoosere et al. (1986) speculated that the digestion of paper and paper sludges could benefit from supplementation of animal manures before digestion in view of the low nitrogen and phosphorous levels.

The quality of OMSW has been shown to affect digester performance, operating at 6% TS. Improvements in microbial activity were observed when separate collection was performed, instead of source separation of the organic fraction (Cecchi et al. 1988).

Six and Debaere (1988) studied the digestion of several different wastes. Their results shown in Table 3 indicate that decomposition of incoming waste was affected by the waste composition as well as by the method of collection. The collection method may introduce greater inerts but may also add

	Initial TS (%)	Loading (kg COD/m ³ r*d)	COD reduction (%)
Mixed MSW	56	17.3	55
Separately collected			
MSW - Duobak	43	20	55
- fruit, veg.+ garden waste	35	10	50
Restaurant waste	19	11	95
Paper Sludge	5	11	55
MSW:WSS 2:1	39	19	56

(Six and DeBaere, 1988)

Table 3: Anaerobic Digestion of Various Organic Wastes

needed nutrients. In Table 3, the mixed MSW at 56% TS achieved the same COD (chemical oxygen demand) reduction as the source separated waste at 43% TS at similar loading rates. This seems to conflict with the findings of Cecchi et al. (1988) reported earlier.

As seen from the other organic wastes listed, COD reduction varies. The separately collected vegetable waste has the lowest COD reduction. This low removal was reported to exist due to the rapid acidification in the reactor (Six and DeBaere, 1988).

Composition of the digestate as reported by various researchers affect digester performance. Rheology of mixing may be a problem when using high paper and cardboard contents (Graindorge et al., 1989). Acidification may exist with pure vegetable wastes (Six and DeBaere, 1988) or there may lack of essential compounds necessary for microbial maintenance and growth.

2.6 End-Product Use

The use of the digested blend of OMSW and sewage sludge has found several applications as a soil conditioner. For use as a soil conditioning agent, the C/N (carbon/nitrogen) ratio has been recommended to be between 10 and 20 (Price and Cheremisinoff, 1981). At this ratio the compost is considered stabilized. At higher C/N ratios carbon and ammonia nitrogen

exert a high oxygen demand, causing septic conditions, which often lead to high acidity levels.

DeBaere et al. (1987) found the anaerobically digested OMSW to have a C/N of 12 to 15 after three weeks of digestion. The cumulative oxygen consumption equalled that of aerobic compost of 4 to 6 months, indicating a high degree of stability. Fecal bacteria were almost completely absent (Debaere et al., 1987). It was the opinion of these researchers that the anaerobically digested OMSW was more hygienic and displayed greater stability than OMSW aerobically composted for 4 months. The net effect was a more desirable soil conditioning agent.

Digested piggery and dairy wastes have been tested successfully as livestock fodder, a component in particle board, and as an agricultural fertilizer (Marchaim and Creden, 1981 in Kimchie et al., 1988).

Sources of heavy metals have been a concern in compost. Heavy metals in the compost have been reduced by 45 to 55% by pre-sorting MSW, thereby avoiding partial solubilization during digestion (Cayrol et al., 1988). If sludge has been added, the quantity of metals and pollutants determines the use of the digestate. Lower quality compost has been used in land reclamation projects.

In addition to compost, biogas results from the fermentation process. One cubic meter of methane at standard temperature and pressure has a net heating value of 35,800

kJ/m^3 (Metcalf and Eddy, 1979). Biogas has a 50 to 65% methane content (DeBaere et al. 1987). With a 55% CH_4 content, digester gas has a heating value of approximately $19,690 \text{ kJ/m}^3$.

2.7 Concluding Remarks

The literature survey above, presents the findings of research in dry anaerobic digestion in municipal solid waste to date. Some results are conclusive such as the importance of mass retention time. The reported effects of temperature are conflicting. Researchers indicate optimum TS, for OMSW anaerobic digestion, may be between 30 and 35%. Digestion of high newspaper-content OMSW has not been adequately addressed to date.

This study attempts to determine the optimum conditions for high solids "dry" anaerobic digestion of typical high cellulosic North American waste.

Operational variables considered in the study were: temperature, solids concentration, MSW:WSS ratio and mass retention time. Performance was evaluated using: biogas productivity, biogas composition, removal efficiency, VFA concentration, pH and alkalinity.

3.0 EXPERIMENTAL METHODS

3.1 Experimental Design

A conservative and economic fractional factorial experimental design (DEXP) was conceived to screen the main variables that could affect the digestion at high TS contents (Montgomery, 1984). The DEXP was made up of four levels of TS (25%, 30%, 35%, and 40%), two levels of temperature (mesophilic at 39 °C and thermophilic at 53 °C), mass retention time (MRT) at two levels (15 and 21 days) and ratio at two levels as well. The ratio is the proportion of total weight of MSW to total weight of WSS in the feed. The responses measured were biogas productivity, percent methane, TS and VS, alkalinity, pH, and VFA concentration.

Table 4 shows the particular set of factors for the 16 reactors used in the DEXP. Several other reactors were operated simultaneously alongside the 16 of the DEXP. Data from these 4, 2 at each temperature, are used where appropriate. These reactors are not incorporated into the analysis of variance (ANOVA) because they were not part of the DEXP set-up. Table 5 lists the additional reactors with their operational factors.

Reactor	Temperature °C	Nominal TS %	Ratio MSW/WSS	Retention Time days
Mesophilic				
M1	39	25	1	21
M2	39	25	2	15
M3	39	40	1	21
M4	39	40	2	15
M5	39	30	1	15
M6	39	35	1	15
M7	39	35	2	21
M8	39	30	2	21
Thermophilic				
T1	53	30	1	21
T2	53	40	1	15
T3	53	40	2	21
T4	53	30	2	15
T5	53	35	1	21
T6	53	35	2	15
T7	53	25	1	15
T8	53	25	2	21

Table 4: Experimental Design Set-up

Reactor	Temperature °C	Nominal TS %	Ratio MSW/WSS	Retention Time days
M0	39	30	2	15
M9	39	20	2	15
T0	53	30	2	21
T9	53	20	2	15

Table 5: Additional Experimental Reactors

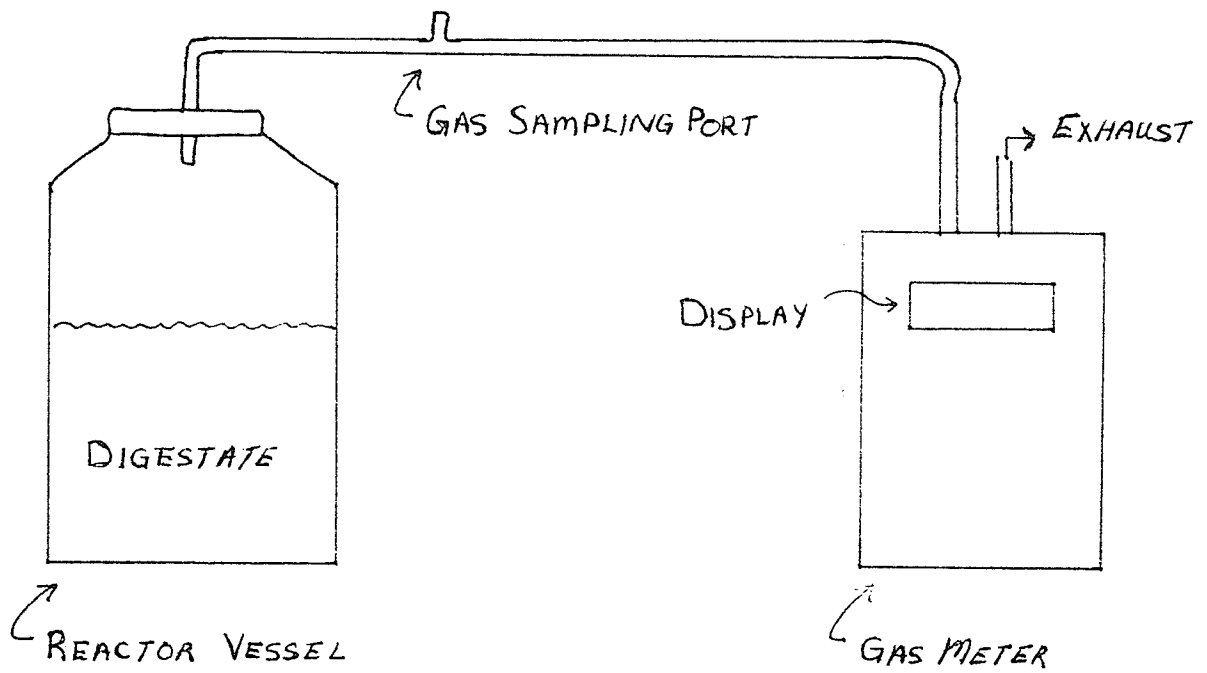


Figure 1: Schematic of Reactor with Gas Meter

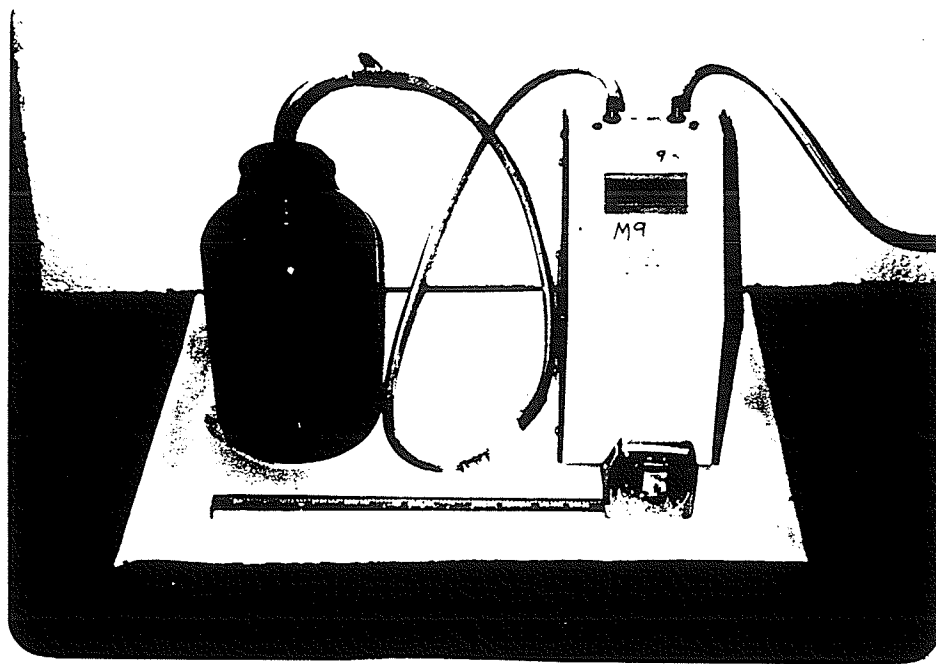


Figure 2: Typical Reactor Set-up

3.2 Reactor Set-up

Each reactor consisted of a glass jar approximately 3 litres in volume. Figure 1 schematically illustrates a reactor with attached gas recording apparatus. Figure 2 is a photograph of a typical reactor set-up. Two separate water baths were maintained at $39\text{ }^{\circ}\text{C} \pm 1\text{ }^{\circ}\text{C}$, mesophilic, and $53\text{ }^{\circ}\text{C} \pm 1\text{ }^{\circ}\text{C}$, thermophilic, using Hach Models E100 and D800 temperature controllers.

3.3 Feed Preparation

A large quantity of semi-synthetic feed was prepared and frozen for use on as-needed basis. The feed consisted of newsprint, food waste, and WSS. Newsprint was shredded to short strips approximately 10 mm by 50 mm in size. Only non-coloured newsprint was used. Food waste was obtained from the campus cafeteria and consisted mainly of discarded prepared breakfast and lunch foods. The blended food waste had a 42% total solids content. The WSS was obtained from the Town of Selkirk storage pond, with a total solids content of 11%. Ratio R1 was defined as a 1:1 MSW:WSS ratio based on total weight. Ratio 1 contained 9.8 parts shredded newsprint to 1.2 parts food waste to 1 part WSS on a total solids basis. Ratio R2 is 2:1 MSW:WSS. Ratio 2 contained 19.7 parts newsprint, 2.3 parts food waste and 1 part WSS on a total solids basis. Newspaper accounted for 89% of the synthetic

OMSW on a TS basis. The food waste accounted for the remaining 11%.

Feed stocks were prepared monthly. Exact feed solids for each reactor were prepared for several feedings, at one time. All feeds were stored in a deep freeze at -20°C and allowed to thaw overnight at 4°C , before feeding. Sodium bicarbonate was added proportionally to the mass loading rate and solids content of the reactor on an as-needed spot basis. Appendix A provides a listing of all NaHCO_3 additions.

3.4 Digester Start-Up

Initial start-up of the digesters was in slurry form. Each digester was seeded with 1 litre anaerobic sludge, obtained from the City of Winnipeg North-End Water Pollution Control Centre digesters. To this, 0.3 litres fresh cow manure, from the University Dairy Sciences and 0.45 litres of prepared OMSW was added. This slurry was flushed with nitrogen gas for 10 minutes before sealing reactor. The weights of each reactor were recorded before and after addition of the start-up mixture.

Each reactor was brought to the specified solids concentration gradually. Prepared substrate was fed twice a week to each reactor. The desired TS content and reactor mass was reached in two retention times, approximately 6 weeks. To ensure stable conditions, an additional six weeks of continuous operation were allowed to pass before the data used for comparative analysis was gathered.

3.5 Feeding

The draw and feed operation was performed on an intermittent basis twice weekly. Later during the study, the draw and feed schedule was reduced to 3 times every two weeks. Oxygen contamination in the reactor was minimized during solids transfer by nitrogen flushing. Reactors were mixed manually by shaking for one minute each day.

3.6 Analysis

A monitoring schedule was developed to determine effectively the status of the anaerobic digesters. The schedule is shown in Table 6.

Biogas production was recorded each morning. Biogas production was measured using a Low Flow Rate Gas Volume Meter Model 181, Triton Electronics Limited, as shown in Figure 2. This meter measured cumulative biogas production by repeated cell volume displacement, with +/- 50 mL accuracy.

In other reactors biogas production was measured by liquid displacement using a saturated NaCl with 5% H₂SO₄ solution.

Preparation of samples for pH, alkalinity, and VFA was based on procedures developed by Kasali et al., 1989. and modified by Poggi et al. 1989. Fifty millilitres of 4 °C deionized water was added to a 10 g sample of solid waste effluent. This slurry was stirred vigorously with glass rod for 15 seconds and allowed to stand 10 minutes in the refrigerator. This sample was stirred once more before pH was

Parameter	Frequency
Biogas Production	daily
Biogas Composition	2/week
pH	2/week
Reactor Mass	2/week
Solids	2/week
Alkalinity	weekly
VFA	weekly
Sodium	biweekly
Ammonia	monthly

Table 6: Analysis Schedule

taken. The pH was measured using a Fisher Accumet Model 230 pH/Ion Meter with a Baxter slimline probe.

Following pH determination the slurry was filtered using a coarse 1.8 mm mesh filter funnel. This filtrate was centrifuged for 15 minutes at 3000 r.p.m. using a Damon/IEC HN-S Centrifuge operating in a 4 °C environmental chamber.

A 20 or 25 ml centrate sample was then taken for alkalinity determination using 0.2 N H₂SO₄ following Standard Methods (A.P.H.A., 1985). Potentiometric points used for phenolphthalein, intermediate and total alkalinity were pH 8.3, 5.75 and 4.2 respectively.

Total solids were determined by drying a 10 g sample 12 hours at 103 °C. Dry samples were ashed at 550 °C for 6 hours to determine volatile solids.

Biogas composition was determined using a Gow Mac 550 gas chromatograph thermal conductivity detector. Helium carrier gas was used at a flowrate of 10 ml/min. Stainless steel 1.8 m by 6 mm columns were packed with Poropak Q, 80/100 mesh to determine methane and carbon dioxide concentrations and Molecular Sieve 5A 60/80 packing, to confirm absence of oxygen. Column temperature was 55 °C, detector temperature 110 °C, injection port temperature 95 °C, and the bridge current 150 mA for both columns.

For volatile fatty acid determination, 1.5 ml of centrate sample was further centrifuged using a high speed IEC Centri-M Centrifuge for 10 minutes. VFA was determined using a Hewlett Packard 5890 Gas Chromatograph thermal conductivity detector. Column used was a HP-FFAP 10 m x 5.3E-4 m x 1.0E-

6 m capillary column. Compressed air was the carrier gas at 13-14 ml/min; nitrogen make-up gas at 7-8 ml/min; H₂ to flame ionization detector (F.I.D) at 30-31 ml/min; air to F.I.D at 450 ml/min. The HP-GC 5890 was programmed to allow VFA to elute in less than 4 minutes with the following temperature program: initial oven temperature 85 °C; initial oven time 1.5 min; initial oven rate 20 deg/min; final temperature 123 °C; final time 1.0 min; rate A 30 deg/min; final temperature A 153 °C; final time A 1.0 minutes. Output was integrated and recorded using a Waters 740 integrator.

4.0 RESULTS AND DISCUSSION

Results of the 10 weeks of steady-state operation have been compiled in Appendix B. Both averages and standard deviations are presented where appropriate. The last 4 weeks of data have been combined where averages are presented. In this period reactors were buffered with sodium bicarbonate on an as-needed basis and reseeded of upset digesters was kept to a minimum. A listing of additions other than regular feed is found in Appendix A. The following discussion will focus mainly on digester averages.

Conventionally, with factorial design experiments (DEXP), design parameters are pooled except the one to be examined. An analysis of variance (ANOVA) table was created to define significance of effects. Table 7 shows the significance of the factor under examination (Hicks, 1982).

Figures 3 through 6 are bar graphs displaying the effects of total solids, temperature, ratio, and retention time respectively. In Figure 3, ratio, retention time and operating temperature are pooled and feed total solids remains as a variable. The same procedure is carried throughout. In Figure 6, the 21 day VFA bar represents an average VFA concentration of all digesters with a 21 day retention time, both mesophilic and thermophilic.

SOURCE	Removal Efficiency	Biogas Production	Volatile Fatty Acids	Volumetric Removal Rate	Removal Rate	Methane
Main Factors:						
Total Solids	v.s.	v.s.	s.	v.s.	v.s.	n.s.
Temperature	m.s.	v.s.	m.s.	v.s.	s.	n.s.
Mass Retention Time	h.s.	s.	h.s.	s.	m.s.	s.
Ratio	s.	v.s.	n.s.	v.s.	s.	w.s.
Interactions:						
TS*T	n.s.	w.s.	n.s.	w.s.	n.s.	n.s.
TS*MRT	n.s.	n.s.	n.s.	n.s.	n.s.	n.s.
TS*MRT*T	n.s.	m.s.	n.s.	m.s.	w.s.	n.s.

note: TS*T*MRT = TS*R

	h.s.	v.s.	s.	m.s.	w.s.	n.s.
	<-----*	<-----*	<-----*	<-----*	<-----*	<-----
	0.01	0.05	0.10	0.15	0.20	

h.s - highly significant
 v.s - very significant
 s - significant
 m.s - moderately significant
 w.s - weakly significant
 n.s - not significant

Table 7: Analysis of Variance

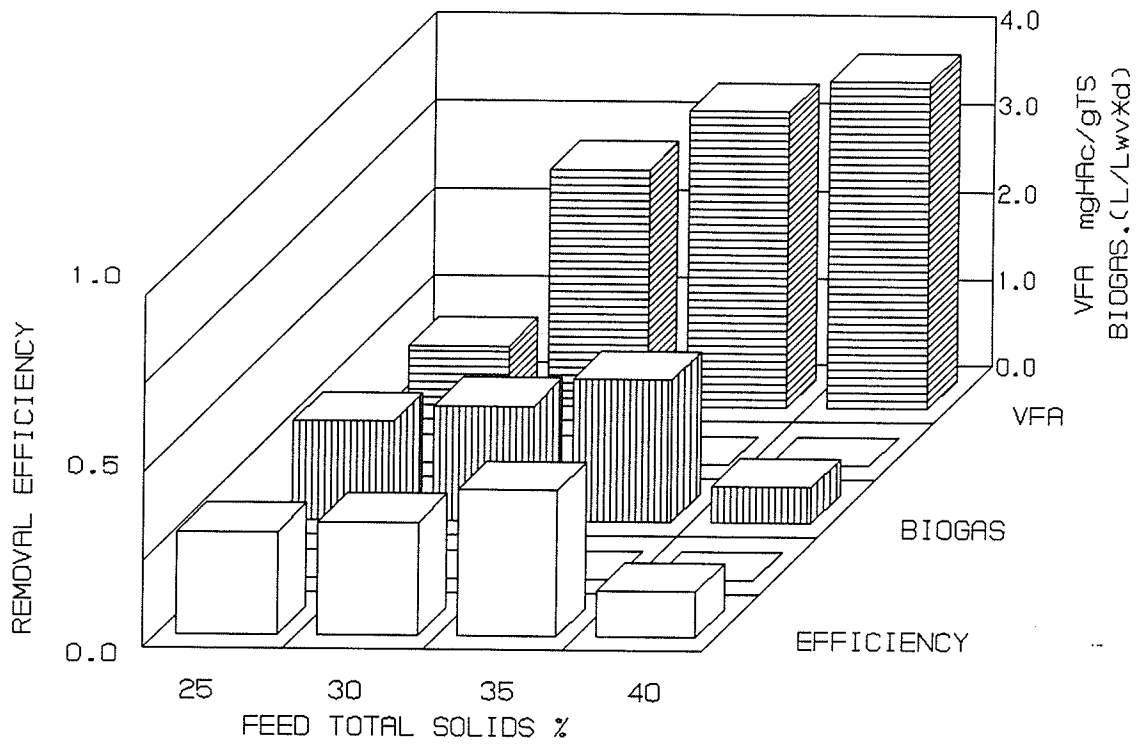


Figure 3: Effect of Total Solids on Responses

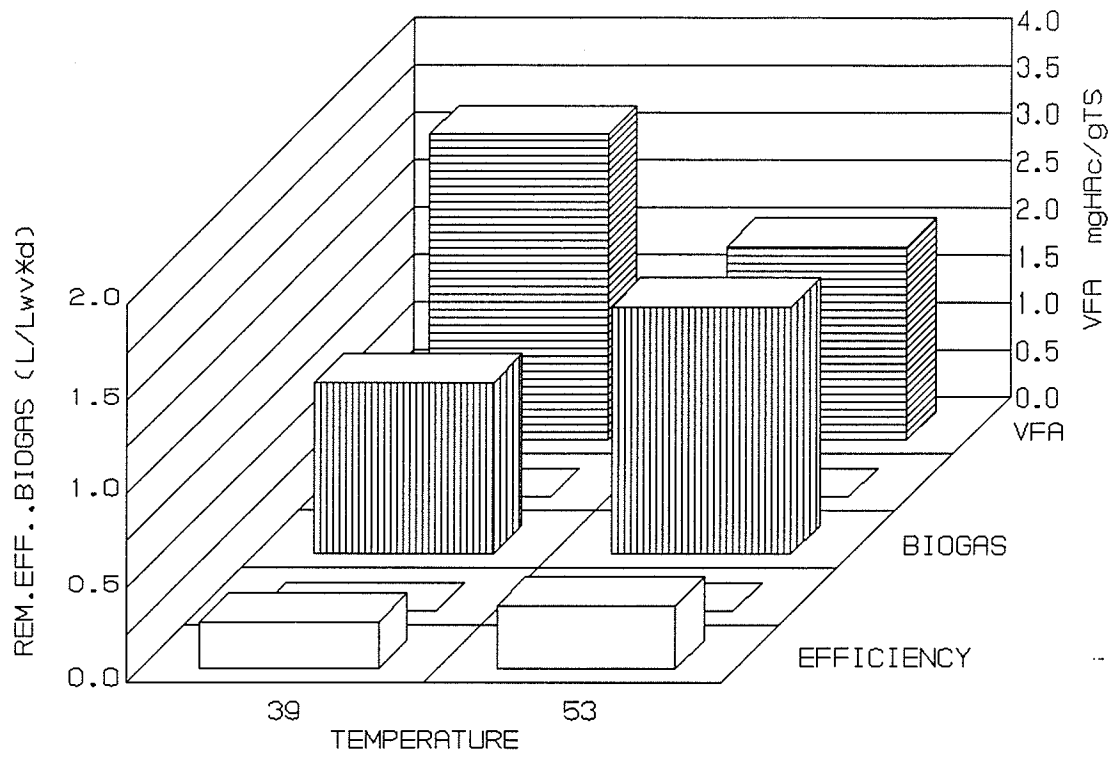


Figure 4: Effect of Temperature on Responses

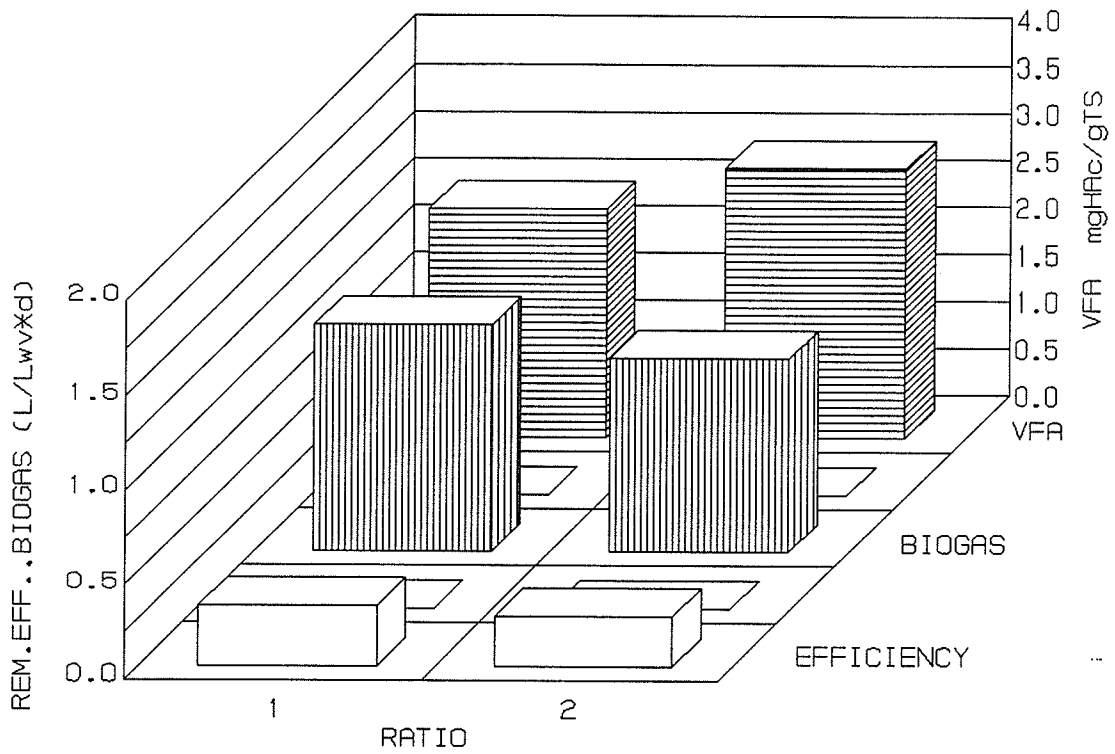


Figure 5: Effect of Ratio on Responses

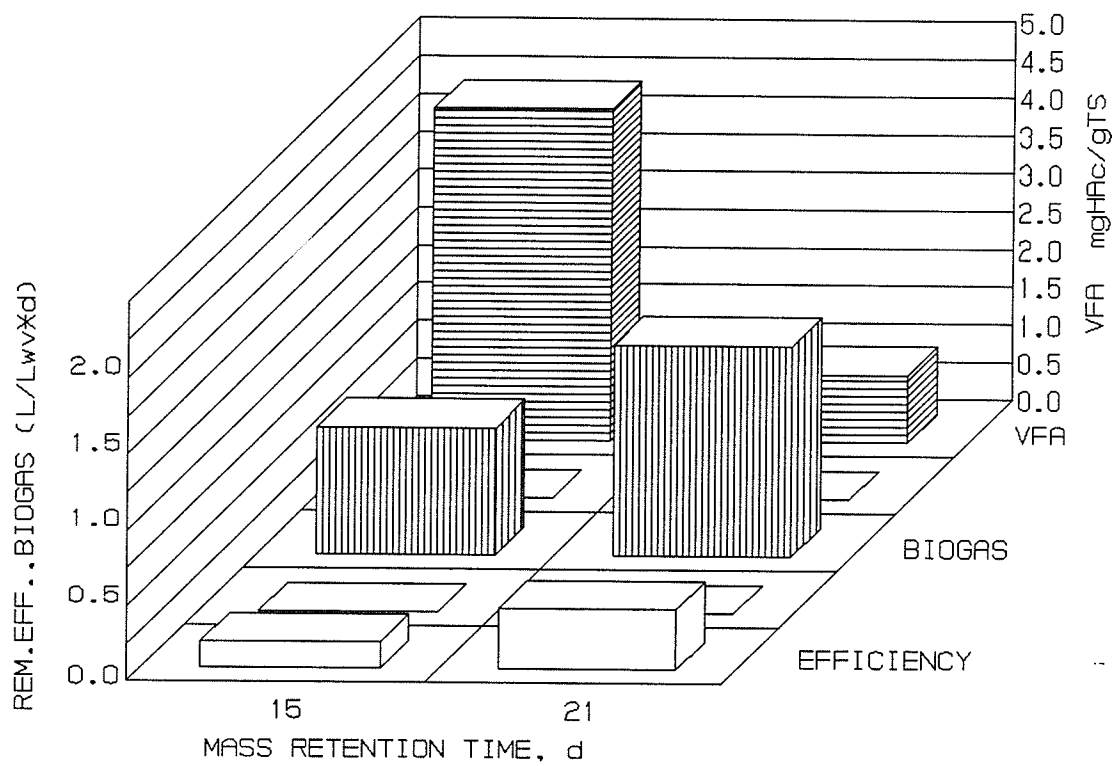


Figure 6: Effect of Retention Time on Responses

4.1 Total Solids

An overview of the solids effect can be seen from the line bars of Figure 3. There did not appear to be a linear effect as might be expected. Efficiency did not decrease linearly with an increase in solids as in sewage sludge. By plotting removal efficiency against feed total solids, there appeared to be a quadratic effect, as shown in Figure 7. There was an optimum experienced somewhere between 30 to 35% TS especially in the 21 day retention time (RT). The 15 day RT did not highlight the solids effect except near 40% where there was a sharp decrease in efficiency.

The effect of total solids on biogas productivity was similar to removal efficiency. Examining Figure 8, a similar optimum was realized between 30 to 35% TS at 21 day RT in both thermophilic and mesophilic. With the shorter retention time of 15 days, there seemed to be a linear effect in productivity followed by a sharp decline in biogas beyond 35% TS. The 25% TS 15 day RT was unexplainably low. This digester experienced several failures and would not operate in a healthy state for extended periods of time. Total solids appeared to have a less significant effect on biogas productivity when accompanied by a shorter retention time.

When ratio of OMSW:WSS was considered as the variable against total solids, as in Figure 9, the results were less clear. The thermophilic ratio 1 (R1) has the greatest biogas productivity. The greater percentage of sludge present aided in higher gas volumes; i.e. greater nutrient supply was

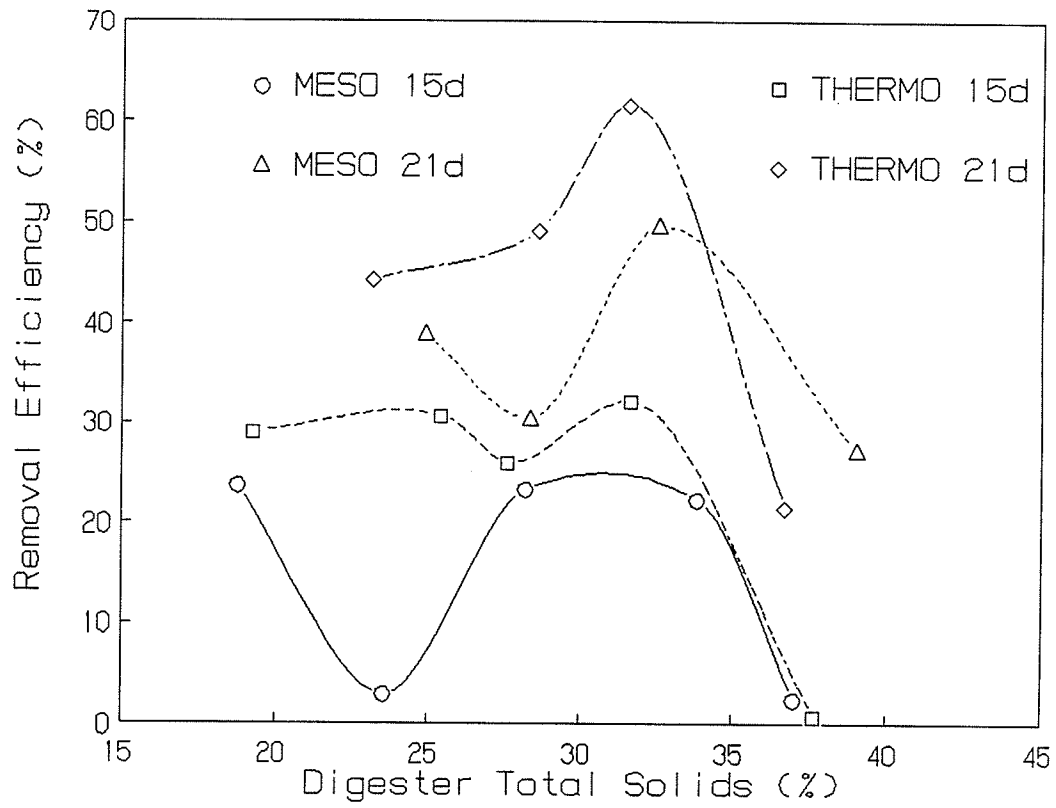


Figure 7: Retention Time, Removal Efficiencies vs Total Solids

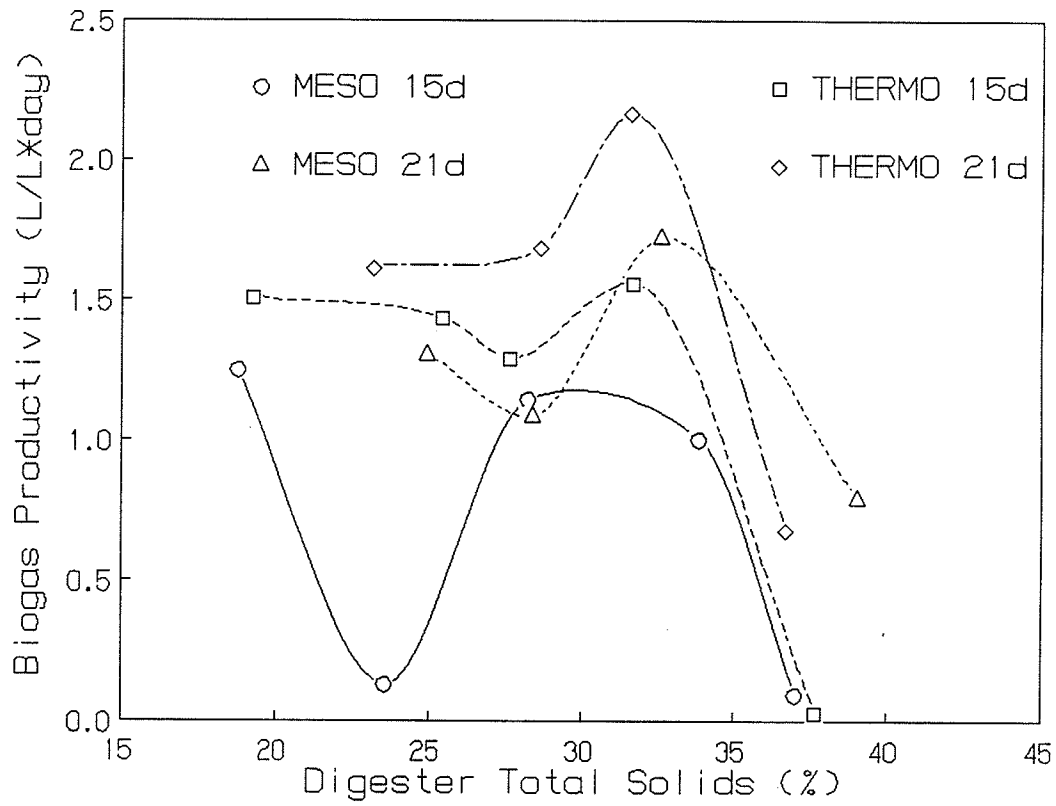


Figure 8: Retention Time, Biogas Productivity vs Total Solids

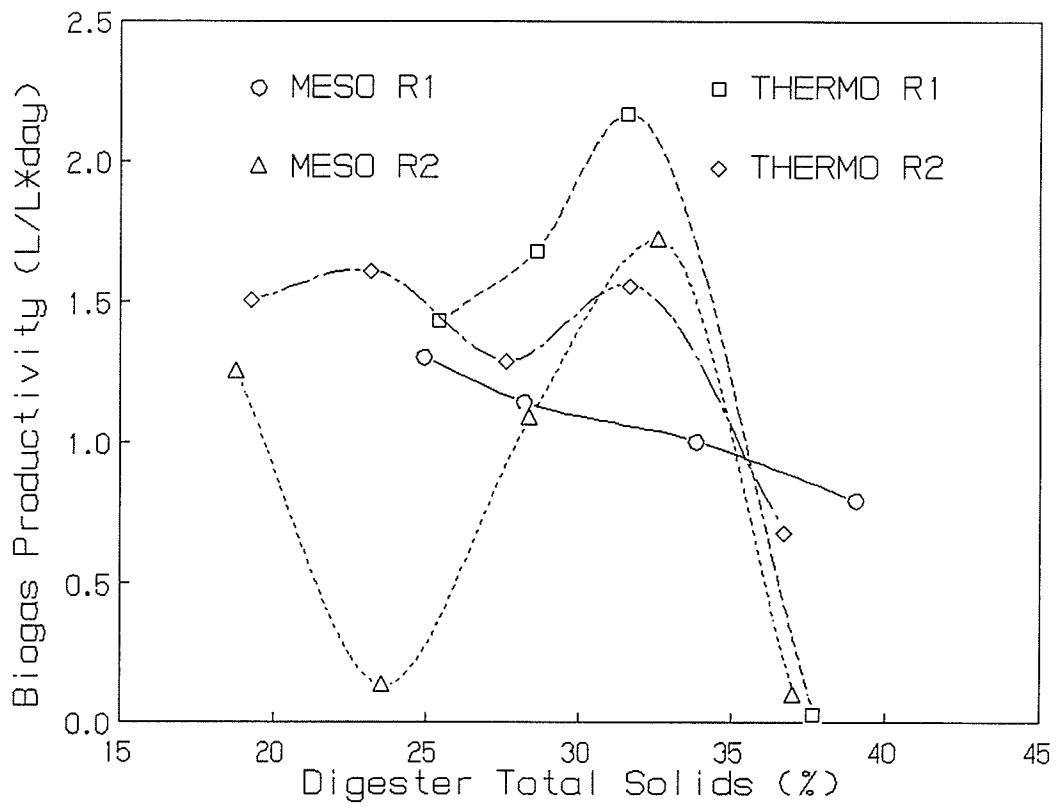


Figure 9: Ratio, Biogas Productivity vs Total Solids

available for microbial maintenance and growth. Thermophilic R2 gave a similar but less significant quadratic effect, with a possible optimum near 25% TS. Peak biogas productivity was 30% less with ratio 2 than with ratio 1.

Figure 3 displays a stepwise increase in VFA concentration with an increase in TS up to 35%. There was less than a 10% increase in VFA from 35 to 40% TS, possibly indicating inhibition to the hydrolysis and acidogenic processes at 40% TS. When this VFA data is examined in greater detail in Figures 10 and 11, it can be seen that the shorter RT contributed most greatly alongside TS to create this build-up in acids. Mesophilic and thermophilic reactors gave similar results at 21 day RT. A low or intermediate level of fatty acids was necessary as a precursor to biogas production. However, a high level of VFA, greater than 4 mg HAC/gTS, inhibited methanogenesis resulting in further acid build-up and eventual failure of the digester.

The 30 to 35% TS range was higher than the optimum experienced for manure substrates, where methane production decreased considerably at 30 to 35 % TS (Wujcik and Jewell, 1980). This optimum was similar to the TS ranges expressed by operators of the Valorga and Dranco processes where a highly fermentable waste was digested (Cayrol et al., 1988; DeBaere, 1985). However, when a high paper and cardboard content OMSW was used (Graindorge et al., 1989), 25% TS was recommended. The addition of WSS, in the present study, may have aided in allowing higher operating solids concentrations.

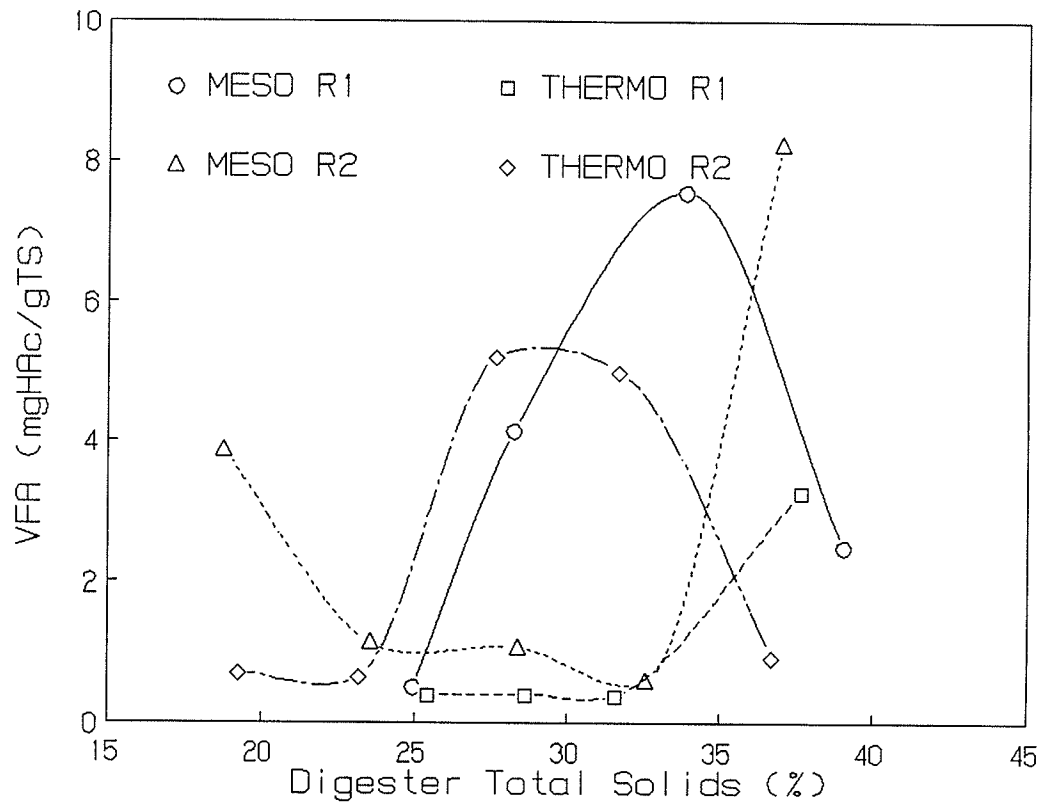


Figure 10: Ratio, Volatile Fatty Acids vs Total Solids

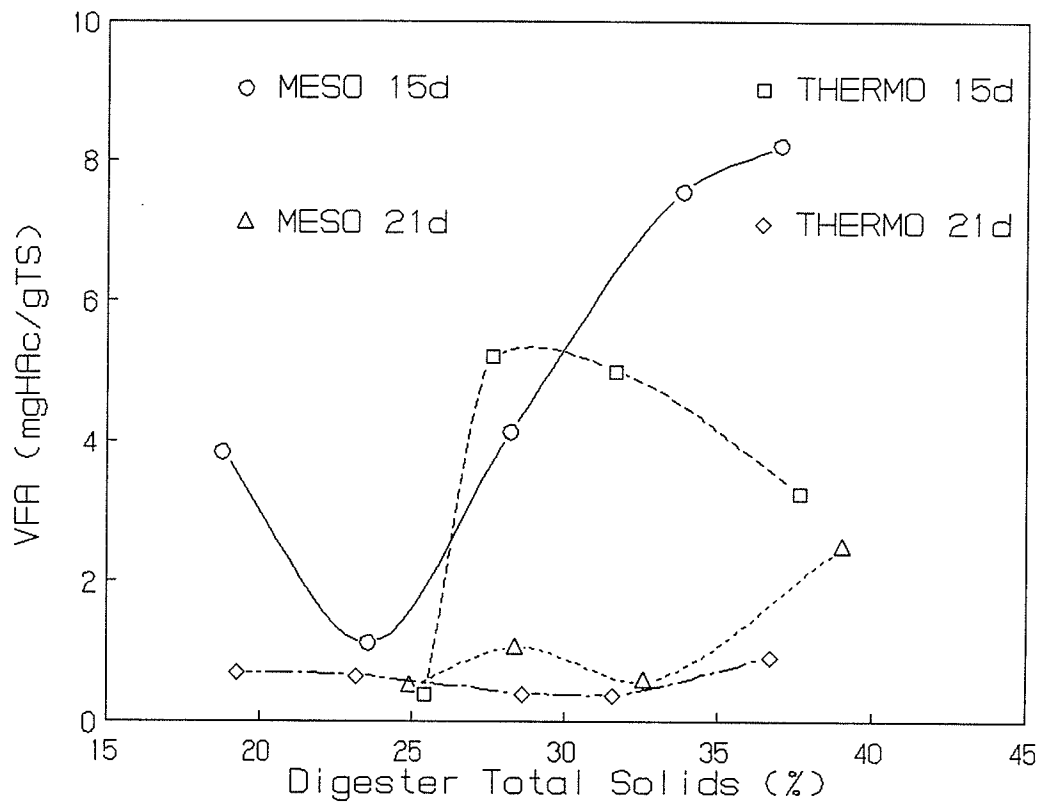


Figure 11: Retention Time, Volatile Fatty Acids vs Total Solids

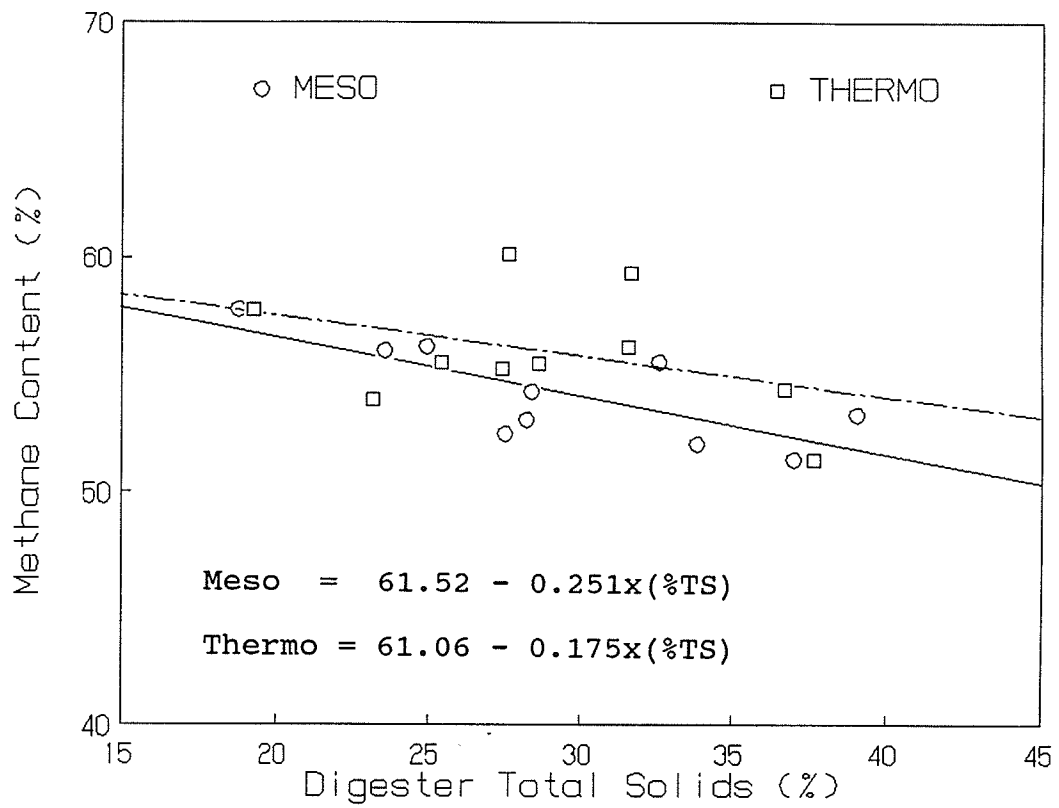


Figure 12: Temperature, Methane Content vs Total Solids

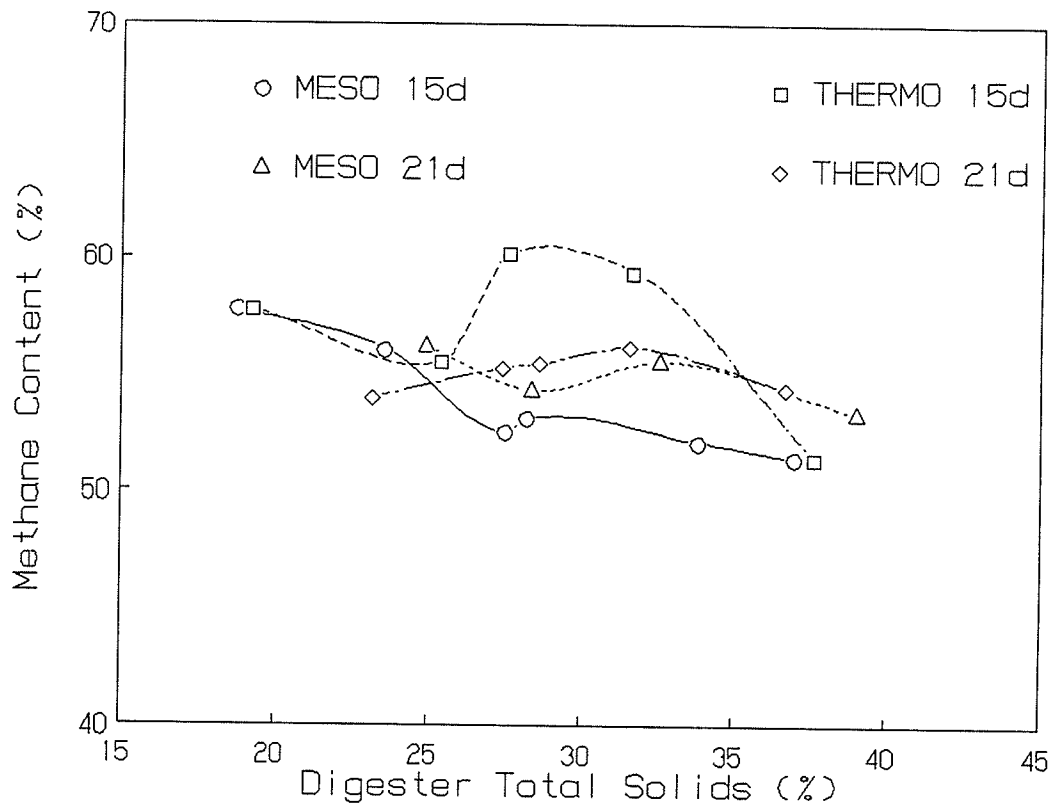


Figure 13: Retention Time, Methane Content vs Total Solids

The effect of TS on methane content was minimal. The average methane concentration ranged from a low of 51.4% to a high of 60.2% CH₄. Some digesters which failed still exhibited high methane values. Graindorge et al. (1989) noted that methane content did not fall in failing digesters. There was a slight decline in methane content with increasing TS. The observed decline was near 5% with a 25% increase in TS. A linear regression performed on the methane contents of all reactors illustrates the low rate of decline with TS increase, Figure 12. There was a slightly higher methane content in both mesophilic and thermophilic 21 day RT digesters (Figure 13), indicating that healthier reactors may have higher methane contents, as one might expect. The slight difference in methane contents indicated however that methane would not be useful in day-to-day monitoring of digester health.

4.2 Temperature

The effects of operating temperature are twofold. An increase in operating temperature, from 39 °C to 53 °C, improved removal efficiency 25%, and biogas production 30%, on average. Average VFA concentration was also reduced (Figure 4). However, process stability was reduced. Several of the thermophilic reactors experienced upsets resulting in low pH, and low biogas production and/or high VFA concentration.

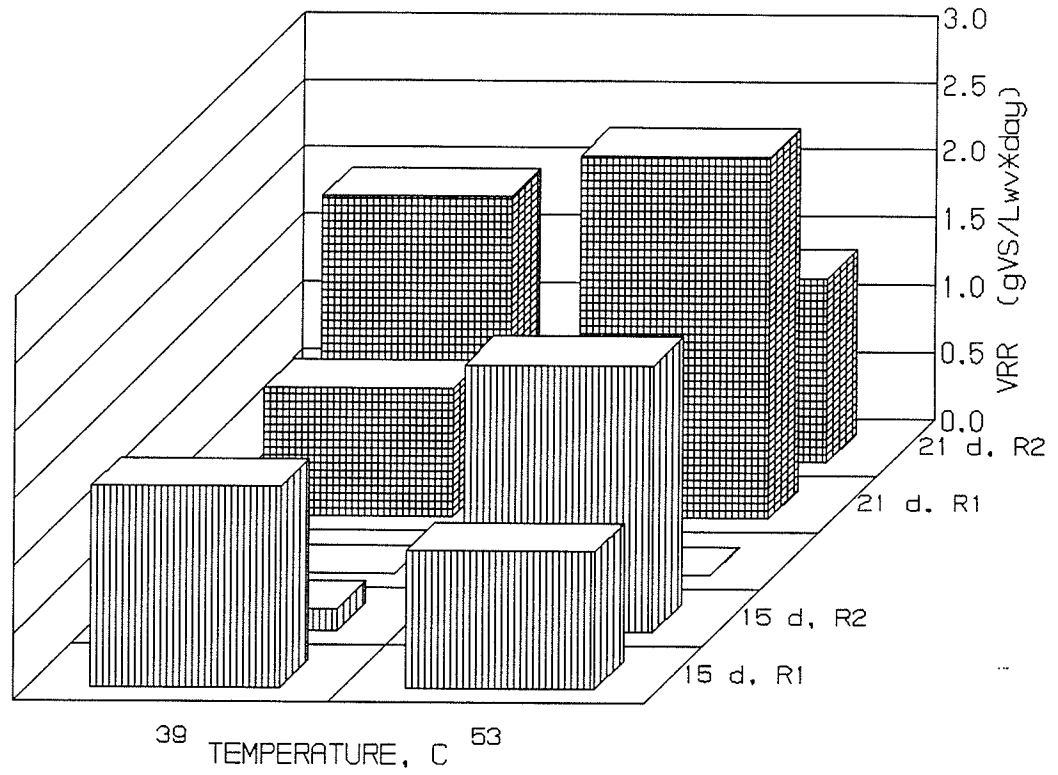


Figure 14: Temperature vs Volumetric Removal Rate

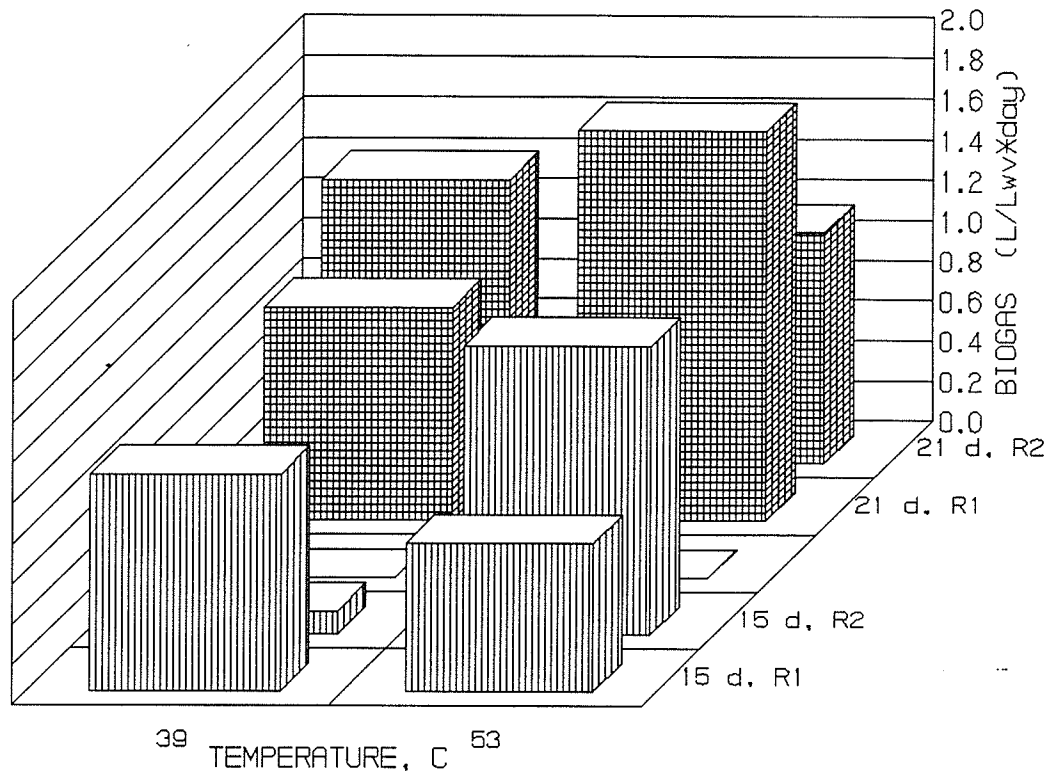


Figure 15: Temperature vs Biogas Productivity

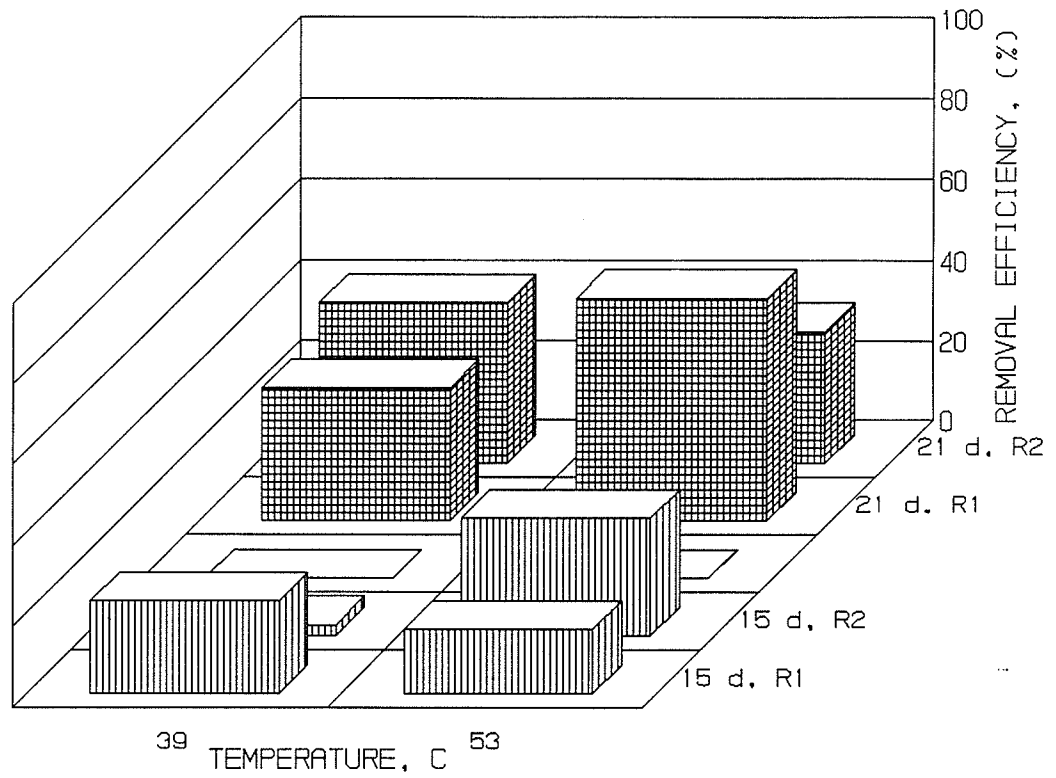


Figure 16: Temperature vs Removal Efficiency

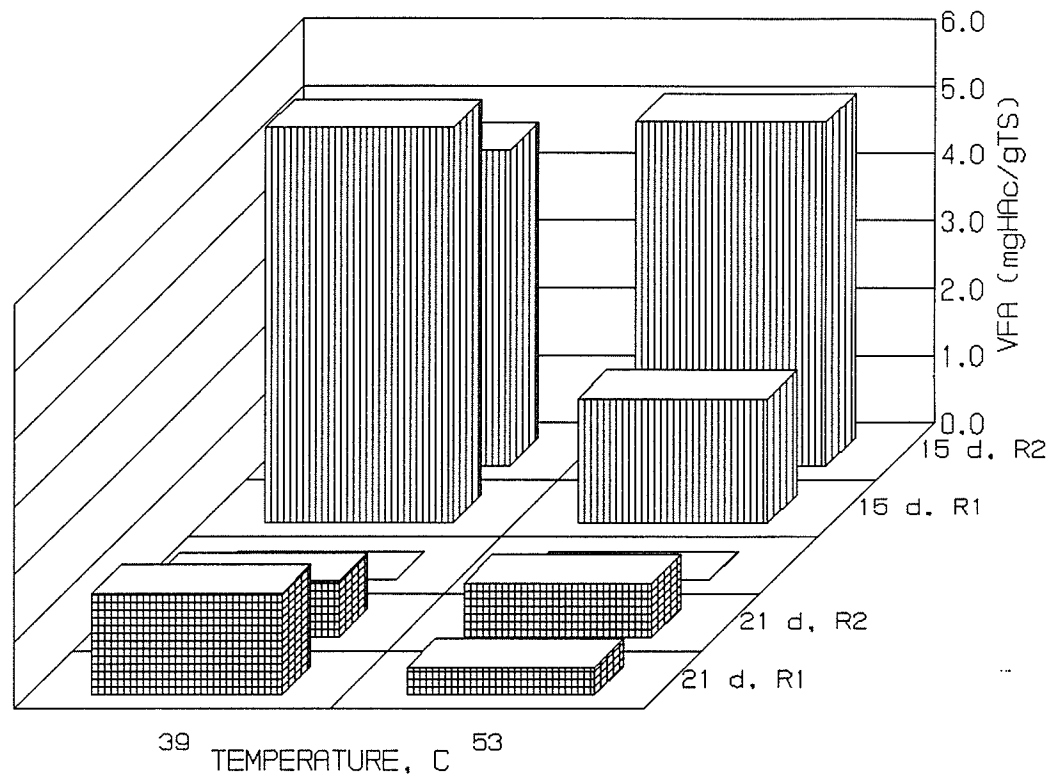


Figure 17: Temperature vs Volatile Fatty Acids

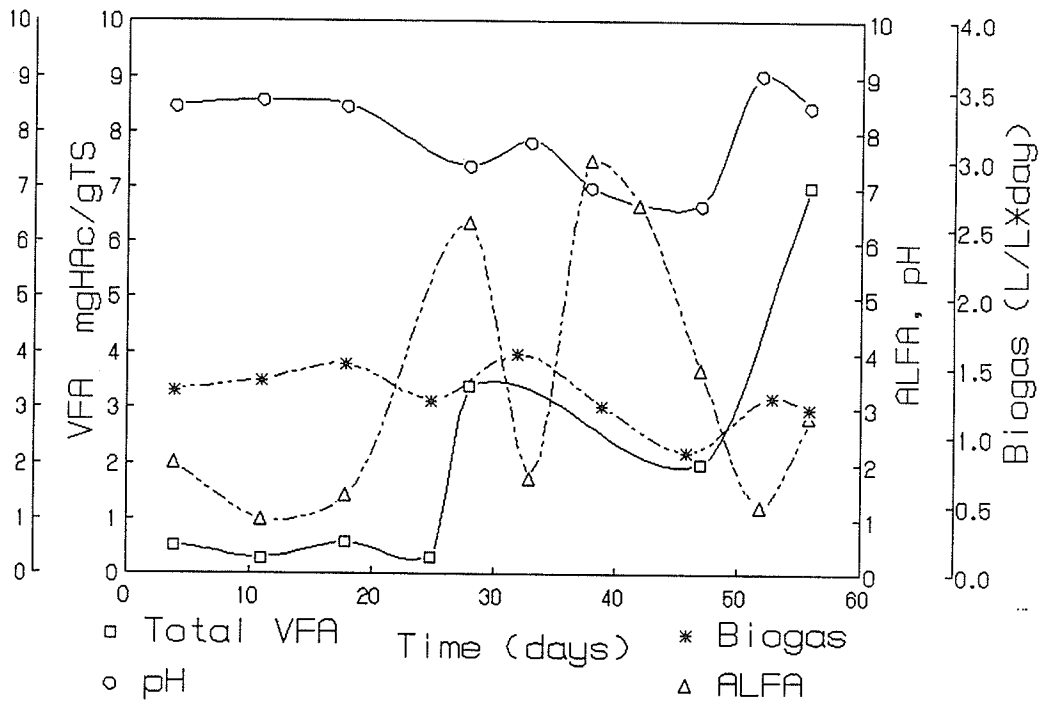


Figure 18: Mesophilic: 30% TS, 15 day RT, R1

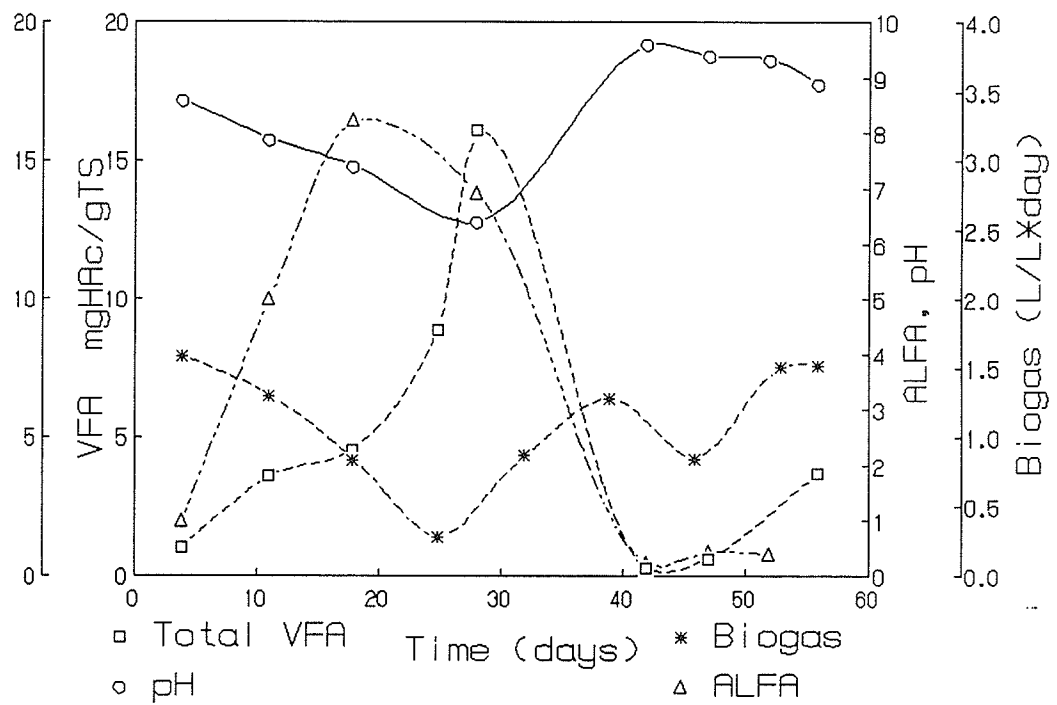


Figure 19: Thermophilic: 30% TS, 15 day RT, R2

In Figure 14 at R1 an increase in temperature resulted in higher removal rates at 21 day RT, yet lower removal rates at 15 day RT. The reverse, however, was true for R2. A decrease in volumetric removal rate was observed at 21 day RT, and a significant increase was seen at 15 day RT, R2.

Comparing the effect of temperature on VFA concentration, the results were more conclusive; see Figure 17. An increase in temperature decreased the VFA level, excepting the case of 15 day RT, R2 where retention time and ratio seemed to have a strong negative effect.

From this study, it is speculated that the thermophilic methanogenic bacteria were more sensitive to the intermittent feeding procedure, lower retention time and/or high cellulosic feed or a combination of the above. Figures 18 and 19, both 30% TS 15 day RT, performed quite differently. The digester M5, ratio 1 represented in Figure 18 was much more stable having never failed. Its responses were more stable than the thermophilic digester, T4 ratio 2, of Figure 19. T4 failed, requiring reseeded on day 25.

While thermophilic digesters at 21 day retention times showed impressive results, caution must be taken. In full scale, both process stability and flexibility are required to withstand changes in substrate quality and variations in loading rates. These operational factors, along with cost, must be taken into account.

4.3 Ratio

The effect of ratio, that is the fraction of WSS present in the OMSW was significant to biogas production and volumetric removal rate (VRR), as shown in Figures 9 and 14. At 30 to 35% TS, thermophilic R1 biogas production exceeded thermophilic R2 by nearly 30%. The differences between mesophilic R1 and R2 are less clear. Ratio 1 displayed an optimum at 25% TS, followed by a decreasing linear effect. Ratio 2 displayed a quadratic optimum at 35% TS. In this study R2 had nearly one-third higher biogas production than R1 in the mesophilic range at 35% TS, but the R1 digesters were more consistent and stable. Table 8 shows the total nitrogen and phosphorous present in the feed. Recalling that R2 had nearly 50% less WSS than R1, it is evident that nutrients came from both the WSS and OMSW. Less than 10% of the TKN (total Kjeldahl nitrogen) came from the OMSW per unit mass. The phosphorous was almost solely derived from the WSS. Ratio, as an indicator of nutrients present, played a role in the performance of the digester. Overall, the operational stability of R1 was greater. WSS is speculated to have supplied nutrients to the microorganisms essential to the degradation process. The VFA contents were nearly 20% higher in R2 digesters, shown in Figure 5. One could speculate that at ratio 2, i.e. higher MSW:WSS, the VFA was greater due to fewer nutrients and more cellulosic supply resulting in a more stressed microbial development.

	TKN	Total
		Phosphorous
	mg N/gTS	mg P/gTS
Ratio 1	3.75	0.89
Ratio 2	2.82	0.58

Nutrient test performed on feed samples 25% TS

Table 8: Feed Nutrient Content

Biomass composition has been described by McCarty as $C_{60}H_{87}O_{23}N_{12}P$. The requirements for nitrogen and phosphorous can then be approximated by the fraction present times the biomass growth. In order for synthesis of new cell growth to proceed, the substrate must contain adequate supply of all the elements which are found in the cytoplasmic material of the cell (Benefield and Randall, 1980). Because the OMSW:WSS substrate was deficient in N and P microbial activity was inhibited.

COD tests indicated that the feed contained approximately 1.1 g COD/gTS. This translates to a COD/N of 300 and 400 for R1 and R2 respectively, indicating nutrient deficiencies. More WSS could be added, if available, to lower COD/N/P ratio and possibly improve digester performance.

4.4 Retention Time

The effects of retention time have been mentioned throughout the discussion of the other parameters. As can be seen in the preceding figures, a longer retention lead to greater process stability and better performance. Figure 6 shows that, on average, an increase in RT from 15 to 21 days lead to more than double the efficiency from 17.6% to 40.1%. Biogas productivity was increased nearly 65% with the increase in retention time.

The 15 day RT reactors exhibited a higher level of upsets. The average VFA concentration was 5 times greater at 15 days than at 21 days. The effect of retention time is highly significant. A MRT of two weeks claimed by some

researchers and processors is not suitable for this situation. A higher MRT is needed to attain reasonable stabilization, efficiencies and reliable operation.

Graindorge and his colleagues came to the conclusion that lengthening the retention time from 17 to 25 days did not improve degradation. This study concurs with most researchers mentioned in the literature review. The MRT has been found to be a significant operational parameter with an optimal retention time near 3 weeks.

4.5 Dynamic Monitoring

Methane content has shown to change only slightly with widely varying digester performance, similar to that experienced by Graindorge et al. (1989). Therefore, methane content was considered to be a poor choice to monitor the health of a digester. In this study, alfa was found suitable for dynamic monitoring. Alfa is defined as:

$$\text{alfa} = \frac{\text{Intermediate Alkalinity (pH 5.75 to 4.20)}}{\text{Partial Alkalinity (initial pH to pH 5.75)}}$$

(Ripley et al., 1986).

An increase in this parameter was related to upcoming stress or failure conditions. As seen in Figure 18 and Figure 19 an increase in VFA was first announced by an increase in alfa. An increase in the alfa parameter can be used to alert remedial action well before an increase in VFA and the resulting decrease in pH and biogas productivity. A low value of alfa indicated a healthy and reliable performance.

5.0 CONCLUSIONS

From the present study examining the co-disposal of waste secondary sludge with synthetic OMSW the following conclusions can be made:

1) The effect of total solids was very significant in the removal efficiency of organic matter and in biogas productivity. Optimim removal efficiency and maximum biogas production were observed between 30 and 35% TS.

2) The effect of retention time was highly significant in VFA concentration as well as process reliability. A 15 day mass retention time affected negatively on the removal efficiency and biogas production. A 21 day MRT resulted in lower VFA concentrations as well as a more reliable and efficient operation.

3) The highest removal efficiencies and biogas production were exhibited by the thermophilic digesters with 21 day RT. The shorter 15 day RT was unstable at the thermophilic operating temperature. Overall, the mesophilic operating temperature was shown to provide greater stability and dependability.

4) Lower MSW:WSS ratio provided microorganisms with more essential nutrients. Digesters fed with ratio 1 MSW:WSS displayed higher removal efficiencies and biogas productivity as well as a lower average VFA concentration.

5) Methane gas content decreased only slightly with decreases in digester performance and was not useful in monitoring the health of the digester.

6) The alfa parameter was an early warning indicator of pending upset or failure.

From the preceding discussion and above conclusions, it is recommended that in the high solids anaerobic digestion of WSS with OMSW that the following parameters be used:

- total solids content of 30 to 35% TS
- mass retention time near 21 days
- a ratio rich in sewage sludge
- mesophilic digesters operating at a temperature of 39 °C to 41 °C.

This set of conditions may be conservative due to the nature of the designed experiment. The operating parameters however will ensure both process flexibility along with reliability and stability in the co-disposal of waste secondary sludge with organic municipal solid waste.

ABBREVIATIONS

ANOVA	Analysis of variance
BG	Biogas
COD	Chemical Oxygen Demand
DAD	Dry anaerobic digestion
DEXP	Experimental design
F.I.D	Flame Ionization Detector
HAc	Acetic acid
MRT	Mass retention time, days
MSW	Municipal solid waste
OMSW	Organic fraction of municipal solid waste
R	Ratio
r	reactor
RR	Removal rate, $\text{gVS}_{\text{removed}}/\text{kgVS}_{\text{contents}} \cdot \text{day}$
RT	Retention Time
T	Temperature, °C
TS	Total solids, % of total weight
VFA	Volatile fatty acids, mg HAc/gTS
VRR	Volumetric removal rate, $\text{gVS}_{\text{removed}}/\text{Lwv} \cdot \text{day}$
VS	Volatile Solids
WSS	waste secondary sludge
wv	working volume of the reactor
w/v	weight per unit volume
w/w	weight per unit weight

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APPENDIX A
FEEDING NOTATIONS

Reactor	Target Mass kg	Feed Mass g*	Feed Mass g**
M0	0.9	210	280
M1	0.5	83	111
M2	0.5	117	156
M3	0.4	67	89
M4	0.4	93	124
M5	0.5	117	156
M6	0.5	117	156
M7	0.5	83	111
M8	0.5	83	111
M9	0.6	140	187
T0	0.9	150	200
T1	0.5	83	111
T2	0.4	93	124
T3	0.4	67	89
T4	0.5	117	156
T5	0.5	83	111
T6	0.5	117	156
T7	0.5	117	156
T8	0.5	83	111
T9	0.6	140	187

* feeding schedule twice per week preceding July 25/89

** feeding schedule three time per two weeks following July 25/89.

SODIUM BICARBONATE AND RESEEDING

July 7	T7	100g of T0
July 12	M4	0.5g Bic.
July 14	M4	2g Bic. + 34g M3 + 50g M7
July 18	T2	2g Bic. + 93g T0
July 25	M0	3.6g Bic.
	M3	0.8g Bic.
	M4	0.8g Bic.
	M6	1g Bic.
	T4	2g Bic.
	T6	2g Bic.
July 28	M0	1g Bic.
	M4	4g Bic.
	T4	2g Bic. + 80g T0
	T5	2g Bic. + 70.3g T0
	T6	2g Bic.
Aug. 2	M2	2g Bic. + 137.2 M0
	M4	2g Bic.
	M6	3g Bic.
Aug. 7	M0	0.5g Bic.
	M1	0.5g Bic.
	M2	2g Bic. + 156g M0
	M3	0.5g Bic.
	M4	79g M7 + 41g M0
	M5	0.5g Bic.
	M6	2g Bic.
	M7	0.5g Bic.
	T2	1g Bic. + 56g T3
	T9	0.5g Bic.
Aug. 11	M0	5.6 Bic.
	M5	0.5 Bic.
	M6	0.5g Bic.
	M7	0.5g Bic.
	M8	0.5g Bic.
	M9	0.5g Bic.
	T2	3.6g Bic. + 111g T0
	T3	1g Bic.
	T8	0.5g Bic.

Aug. 16 M0 3.6g Bic.
M2 151.3g M
M3 0.5g Bic.
M4 79.6g M
M5 0.5g Bic.
M6 1g Bic.
M7 0.5g Bic.
M8 2g Bic.
M9 2.4g Bic.
T2 77.4 T.
T3 1g Bic.
T8 0.5g Bic.

Aug. 21 restart T2: 100g T2 + 183g T0 + 46g T3 + 72g T1

M0 1.4g Bic.
M1 0.33g Bic.
M2 0.47c Bic.
M3 0.27g Bic.
M4 0.37g Bic.
M5 0.47g Bic.
M6 0.78g Bic.
M7 0.56g Bic.
M8 0.56g Bic.
M9 0.56g Bic.
T0 0.60g Bic.
T1 0.11g Bic.
T2 0.62g Bic.
T3 0.44g Bic.
T4 0.47g Bic.
T5 0.33g Bic.
T6 0.78g Bic.
T7 0.47g Bic.
T8 0.33g Bic.
T9 0.56g Bic.

APPENDIX B
OPERATIONAL DATA

B1: PERFORMANCE DATA

SAMPLE	Mass of Reactor (kg)	Retention Time days	Ratio	Nominal Total Solids %	Average Total Solids %	Mass of Reactor (kgTS)	Mass of Reactor (kgVS)	Bulk Density (kg/L)	Digest Volume (L)
M0	0.9	15	2	30	27.55	0.248	0.235	0.428	2.10
M1	0.5	21	1	25	24.95	0.125	0.118	0.466	1.07
M2	0.5	15	2	25	23.59	0.118	0.114	0.487	1.03
M3	0.4	21	1	40	39.09	0.156	0.149	0.257	1.56
M4	0.4	15	2	40	37.05	0.148	0.144	0.287	1.39
M5	0.5	15	1	30	28.28	0.141	0.134	0.417	1.20
M6	0.5	15	1	35	33.91	0.170	0.161	0.334	1.50
M7	0.5	21	2	25	32.55	0.163	0.159	0.353	1.42
M8	0.5	21	2	30	28.47	0.142	0.138	0.414	1.21
M9	0.6	15	2	20	18.83	0.113	0.110	0.557	1.08
T0	0.9	21	2	30	27.45	0.247	0.240	0.429	2.10
T1	0.5	21	1	30	28.66	0.143	0.136	0.412	1.22
T2	0.4	15	1	40	37.69	0.151	0.143	0.278	1.44
T3	0.4	21	2	40	36.78	0.147	0.143	0.291	1.37
T4	0.5	15	2	30	27.69	0.138	0.135	0.426	1.17
T5	0.5	21	1	35	31.63	0.158	0.150	0.368	1.36
T6	0.5	15	2	35	31.72	0.159	0.154	0.366	1.37
T7	0.5	15	1	25	25.50	0.127	0.121	0.458	1.09
T8	0.5	21	2	25	23.25	0.116	0.113	0.492	1.02
T9	0.6	15	2	20	19.34	0.116	0.112	0.549	1.09

SAMPLE	Input g/day	Input TS g/day	Input VS g/day	JULY AVERAGE (L/day)	AUGUST AVERAGE (L/day)	Jul-Aug AVERAGE (L/day)
M0	60.00	18.29	17.78	1.622	1.930	1.759
M1	23.81	5.30	5.01	1.359	1.399	1.377
M2	33.33	6.87	6.42	1.067	0.138	0.654
M3	19.05	6.72	6.32	1.288	1.238	1.266
M4	26.67	8.23	7.86	1.199	0.140	0.728
M5	33.33	8.67	8.19	1.707	1.374	1.559
M6	33.33	9.99	9.38	1.341	1.505	1.414
M7	23.81	7.06	6.84	2.129	2.443	2.269
M8	23.81	6.19	5.99	1.631	1.311	1.489
M9	40.00	8.18	7.89	1.676	1.347	1.530
T0	42.86	13.07	12.70	2.382	1.789	2.118
T1	23.81	6.13	5.81	2.057	2.052	2.055
T2	26.67	9.06	8.63	0.742	0.054	0.436
T3	19.05	6.29	6.07	1.096	0.939	1.026
T4	33.33	8.39	8.11	1.149	1.517	1.313
T5	23.81	7.07	6.65	2.563	2.954	2.737
T6	33.33	9.54	9.21	1.253	2.133	1.644
T7	33.33	7.48	7.08	1.489	1.567	1.524
T8	23.81	5.32	5.15	1.295	1.644	1.450
T9	40.00	8.18	7.89	1.817	1.648	1.742

SAMPLE	(Yield= 0.72 m ³ /kgVS rem.)			Volumetric	Mass
	JULY	AUGUST	Jul-Aug	Loading Rate (gVSfed/ Lwv*d)	Loading Rate (gVSfed/ kgMass*d) (gVSfed/ kgMvs*d)
	Efficiency	Efficiency	Efficiency		
M0	0.127	0.151	0.137	8.46	19.76 75.75
M1	0.377	0.388	0.382	4.67	10.02 42.42
M2	0.231	0.030	0.141	6.25	12.84 56.18
M3	0.283	0.272	0.278	4.06	15.80 42.52
M4	0.212	0.025	0.129	5.64	19.65 54.55
M5	0.289	0.233	0.264	6.83	16.38 61.13
M6	0.199	0.223	0.209	6.26	18.76 58.33
M7	0.432	0.496	0.461	4.82	13.68 43.10
M8	0.378	0.304	0.345	4.96	11.98 43.30
M9	0.295	0.237	0.269	7.33	13.15 71.86
T0	0.261	0.196	0.232	6.05	14.11 52.89
T1	0.492	0.491	0.491	4.78	11.62 42.79
T2	0.119	0.009	0.070	6.00	21.58 60.23
T3	0.251	0.215	0.235	4.42	15.18 42.44
T4	0.197	0.260	0.225	6.91	16.22 60.28
T5	0.535	0.617	0.572	4.89	13.30 44.34
T6	0.189	0.322	0.248	6.75	18.42 59.73
T7	0.292	0.307	0.299	6.49	14.16 58.67
T8	0.349	0.443	0.391	5.06	10.30 45.72
T9	0.320	0.290	0.307	7.22	13.15 70.18

SAMPLE	July	August	Jul-Aug	July	August	Jul-Aug
	Removal Rate (gVS/kgVS*d)			Volumetric Removal Rate (gVS/Lvw*d)		
M0	9.598	11.421	10.408	1.071	1.275	1.162
M1	15.985	16.452	16.192	1.759	1.811	1.782
M2	12.965	1.672	7.946	1.442	0.186	0.884
M3	12.035	11.570	11.828	1.149	1.105	1.130
M4	11.556	1.346	7.018	1.195	0.139	0.726
M5	17.693	14.241	16.159	1.977	1.591	1.806
M6	11.581	12.998	12.211	1.244	1.396	1.311
M7	18.633	21.379	19.854	2.085	2.393	2.222
M8	16.374	13.165	14.948	1.876	1.508	1.712
M9	21.199	17.030	19.346	2.161	1.736	1.972
T0	13.779	10.344	12.253	1.577	1.184	1.402
T1	21.041	20.993	21.020	2.351	2.346	2.349
T2	7.189	0.520	4.225	0.716	0.052	0.421
T3	10.642	9.120	9.965	1.107	0.949	1.037
T4	11.865	15.659	13.551	1.360	1.795	1.553
T5	23.731	27.351	25.340	2.620	3.019	2.797
T6	11.288	19.215	14.811	1.275	2.171	1.673
T7	17.138	18.039	17.539	1.896	1.996	1.940
T8	15.972	20.269	17.882	1.769	2.245	1.981
T9	22.444	20.350	21.513	2.309	2.094	2.213

SAMPLE	JULY AVERAGE			AUGUST AVERAGE			JUL-AUG AVERAGE		
	Yield	Yield	Yield	Yield	Yield	Yield	Yield	Yield	Yield
	(m ³ BG/ kg.fed)	(m ³ BG/ kgTSfed)	(m ³ BG/ kgVSfed)	(m ³ BG/ kg.fed)	(m ³ BG/ kgTSfed)	(m ³ BG/ kgVSfed)	(m ³ BG/ kg.fed)	(m ³ BG/ kgTSfed)	(m ³ BG/ kgVSfed)
M0	0.027	0.089	0.091	0.032	0.106	0.109	0.029	0.096	0.099
M1	0.057	0.256	0.271	0.059	0.264	0.279	0.058	0.260	0.275
M2	0.032	0.155	0.166	0.004	0.020	0.021	0.020	0.095	0.102
M3	0.068	0.192	0.204	0.065	0.184	0.196	0.066	0.188	0.200
M4	0.045	0.146	0.153	0.005	0.017	0.018	0.027	0.088	0.093
M5	0.051	0.197	0.208	0.041	0.158	0.168	0.047	0.180	0.190
M6	0.040	0.134	0.143	0.045	0.151	0.160	0.042	0.142	0.151
M7	0.089	0.302	0.311	0.103	0.346	0.357	0.095	0.321	0.332
M8	0.069	0.263	0.272	0.055	0.212	0.219	0.063	0.241	0.249
M9	0.042	0.205	0.212	0.034	0.165	0.171	0.038	0.187	0.194
T0	0.056	0.182	0.188	0.042	0.137	0.141	0.049	0.162	0.167
T1	0.086	0.336	0.354	0.086	0.335	0.353	0.086	0.335	0.354
T2	0.028	0.082	0.086	0.002	0.006	0.006	0.016	0.048	0.051
T3	0.058	0.174	0.181	0.049	0.149	0.155	0.054	0.163	0.169
T4	0.034	0.137	0.142	0.046	0.181	0.187	0.039	0.156	0.162
T5	0.108	0.362	0.385	0.124	0.418	0.444	0.115	0.387	0.412
T6	0.038	0.131	0.136	0.064	0.224	0.232	0.049	0.172	0.179
T7	0.045	0.199	0.210	0.047	0.210	0.221	0.046	0.204	0.215
T8	0.054	0.244	0.252	0.069	0.309	0.319	0.061	0.273	0.282
T9	0.045	0.222	0.230	0.041	0.201	0.209	0.044	0.213	0.221

JUL-AUG 1989 Sample	VFA	VFA	VFA	VFA	VFA	VFA	VFA	VFA	Average Std. Dev.	
	as HAc	as HAc	as HAc	as HAc	as HAc	as HAc	as HAc	as HAc	4/7-25/8	4/7-25/8
	(mg/g) 4/7	(mg/g) 11/7	(mg/g) 18/7	(mg/g) 25/7	(mg/g) 29/7	(mg/g) 11/8	(mg/g) 16/7	(mg/g) 25/6	VFA as HAc (mg/g)	VFA as HAc (mg/g)
M0	1.32	0.02	1.80	2.51	4.85		4.02	16.03	4.36	5.00
M1	0.51	0.96	0.99	0.33	0.58		0.48	0.46	0.56	0.24
M2	0.84	0.37	0.54	0.21	1.13		0.00	2.23	0.78	0.58
M3	0.81	0.45	0.66	0.33	2.50		1.18	3.82	1.39	1.20
M4	1.29	0.59		8.28	10.66		4.63	9.38	5.81	3.90
M5	0.54	0.32	0.59	0.34	3.40		2.01	7.04	2.04	2.30
M6	1.14	1.22	1.53	2.30	4.13		5.42	13.20	4.13	3.99
M7	0.59	0.79	0.51		0.58		0.14	1.05	0.63	0.27
M8	0.72	0.92	0.90	0.27	0.43		0.49	2.27	0.86	0.62
M9	0.59	0.94	0.98		0.89		1.67	9.01	2.35	3.00
T0	0.27	0.63	0.45		0.67	1.51	0.06	4.48	1.15	1.42
T1	0.70	0.23	0.26		0.62	0.42	0.53	0.00	0.41	0.24
T2	2.06	3.08	5.20	3.06		4.17	2.71	3.00	3.33	0.96
T3	1.15	0.54	1.27	0.77	0.78	0.00	1.07	1.92	0.95	0.52
T4	1.09	3.62	4.59	3.92	16.15	0.30	0.67	2.77	4.89	4.99
T5	0.00	0.36	3.74		0.48	0.54	0.05	0.54	0.82	1.21
T6	0.65	3.89	6.53		16.84	0.46	0.70	1.98	4.44	5.46
T7	0.54	0.69	0.55		0.57	0.21	0.03	0.83	0.49	0.26
T8	0.66	0.19	0.00	0.63	0.46	0.27		1.26	0.46	0.38
T9	0.68	0.70	0.38		0.47	0.29		1.38	0.65	0.36
F R1;25	4.59	7.31	1.73					0.47	3.53	2.65
F R1;30	6.67	5.16	2.54					0.72	3.77	2.30
F R1;35	4.05	4.66	1.58					0.79	2.77	1.62
F R1;40	2.81	2.47	1.26					0.65	1.90	0.88
F R2;20	7.86	9.96	4.99					1.46	6.07	3.20
F R2;25	3.51	2.91	2.39					0.94	2.43	0.95
F R2;30	1.35	3.46	2.52					0.59	1.98	1.10
F R2;35	3.37	5.00	2.29					1.20	2.96	1.41
F R2;40	0.22	2.79	2.77					1.51	1.82	1.06

B2: BIOGAS PRODUCTIVITY AND COMPOSITION

SAMPLE	Mass of Reactor (kg)	Nominal Total Solids %	Average Total Solids %	Mass of Reactor (kgTS)	Bulk Density (kg/L)	Digest Volume (L)
M0	0.900	30	27.55	0.248	0.428	2.10
M1	0.500	25	24.95	0.125	0.466	1.07
M2	0.500	25	23.59	0.118	0.487	1.03
M3	0.400	40	39.09	0.156	0.257	1.56
M4	0.400	40	37.05	0.148	0.287	1.39
M5	0.500	30	28.28	0.141	0.417	1.20
M6	0.500	35	33.91	0.170	0.334	1.50
M7	0.500	35	32.65	0.163	0.353	1.42
M8	0.500	30	28.47	0.142	0.414	1.21
M9	0.600	20	18.83	0.113	0.557	1.08
T0	0.900	30	27.45	0.247	0.429	2.10
T1	0.500	30	28.66	0.143	0.412	1.22
T2	0.400	40	37.69	0.151	0.278	1.44
T3	0.400	40	36.78	0.147	0.291	1.37
T4	0.500	30	27.69	0.138	0.426	1.17
T5	0.500	35	31.63	0.158	0.368	1.36
T6	0.500	35	31.72	0.159	0.366	1.37
T7	0.500	25	25.50	0.127	0.458	1.09
T8	0.500	25	23.25	0.116	0.492	1.02
T9	0.600	20	19.34	0.116	0.549	1.09

AVERAGE DAILY BIOGAS PRODUCTION PER REACTOR @ STP

SAMPLE	28/6-4/7	5/7-11/7	12/7-18/7	19/7-25/7	26/7-1/8	2/8-8/8	9/8-15/8	16/8-22/8	23/8-25/8
	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)
M0	1.737	1.327	1.443	1.205	1.899	1.648	1.898	2.397	1.378
M1	1.365	1.797	1.404	0.709	1.502	1.457	1.445	1.369	1.325
M2	1.314	2.086	0.726	0.710	0.298	0.072	0.000	0.337	0.142
M3	1.301	1.209	1.210	1.195	1.524	1.353	1.152	1.210	1.228
M4	1.337	1.126	1.500	1.281	0.751	0.234	0.088	0.148	0.088
M5	1.539	1.588	1.818	1.515	1.914	1.456	1.366	1.538	1.435
M6	1.468	1.275	1.327	1.236	1.397	1.765	1.636	1.552	1.067
M7	1.557	1.814	2.123	2.681	2.471	2.385	2.602	2.530	2.254
M8	1.604	1.641	1.752	1.634	1.524	1.185	1.119	1.568	1.374
M9	1.526	1.885	1.658	1.897	1.415	1.142	0.962	1.822	1.460
T0	2.504	2.167	1.967	2.357	2.917	2.576	1.661	1.625	1.292
T1	1.966	2.530	2.293	1.216	2.280	2.016	2.215	2.099	1.878
T2	1.375	1.228	0.335	0.315	0.456	0.074	0.074	0.020	0.047
T3	1.311	1.356	1.019	0.821	0.973	0.775	0.749	1.281	0.951
T4	1.864	1.525	0.988	0.338	1.033	1.504	1.007	1.772	1.785
T5	2.259	2.946	2.500	2.386	2.822	3.023	3.083	3.144	2.565
T6	2.178	1.042	1.167	0.412	1.467	2.066	1.667	2.572	2.229
T7	1.917	1.420	1.254	1.193	1.662	1.331	1.371	1.708	1.859
T8	1.702	1.464	1.188	1.012	1.111	1.084	0.973	2.188	2.331
T9	1.698	2.279	1.737	1.774	1.597	1.428	1.833	1.560	1.769

SAMPLE	JULY		AUGUST		JUL-AUG	
	AVERAGE (L/day)	Std. Dev. (L/day)	AVERAGE (L/day)	Std. Dev. (L/day)	AVERAGE (L/day)	Std. Dev. (L/day)
M0	1.622	0.260	1.930	0.297	1.759	0.317
M1	1.359	0.357	1.399	0.055	1.377	0.269
M2	1.067	0.644	0.138	0.125	0.654	0.671
M3	1.288	0.124	1.238	0.071	1.266	0.107
M4	1.199	0.254	0.140	0.059	0.728	0.561
M5	1.707	0.144	1.374	0.182	1.559	0.232
M6	1.341	0.084	1.505	0.264	1.414	0.204
M7	2.129	0.412	2.443	0.134	2.269	0.356
M8	1.631	0.073	1.311	0.175	1.489	0.205
M9	1.676	0.192	1.347	0.327	1.530	0.308
T0	2.382	0.323	1.789	0.477	2.118	0.496
T1	2.057	0.457	2.052	0.123	2.055	0.351
T2	0.742	0.462	0.054	0.022	0.436	0.485
T3	1.096	0.205	0.939	0.212	1.026	0.222
T4	1.149	0.520	1.517	0.315	1.313	0.477
T5	2.563	0.234	2.954	0.228	2.737	0.302
T6	1.253	0.576	2.133	0.325	1.644	0.650
T7	1.489	0.268	1.567	0.223	1.524	0.252
T8	1.295	0.253	1.644	0.619	1.450	0.486
T9	1.817	0.238	1.548	0.162	1.742	0.224

PERCENT METHANE CONTENT

SAMPLE	3/7	6/7	17/7	24/7	27/7	1/8	10/8	15/8
	CH4 %	CH4 %	CH4 %	CH4 %	CH4 %	CH4 %	CH4 %	CH4 %
M0	51.0	52.9	52.1	51.2	53.2	55.3	48.6	52.6
M1	52.8	53.0	52.2	53.3	56.7	59.2	53.8	55.7
M2	53.8	55.6	55.3	54.3	49.2	60.2	50.1	56.0
M3	51.9	52.9	51.2	53.2	55.2	56.4	50.7	52.7
M4	51.3	50.7	47.0	49.3	49.5	53.5	46.3	52.4
M5	49.4	52.9	53.8	53.9	58.3	57.4	50.4	51.6
M6	51.1	51.9	51.7	50.6	56.6	54.0	46.1	55.2
M7	52.2	52.9	54.3	53.8	59.1	58.2	52.2	56.3
M8	52.8	53.6	53.8	54.4	61.8	58.4	50.8	53.6
M9	53.3	53.9	53.1	53.3	59.1	58.4	50.4	64.7
T0	54.3	55.7	55.3	54.7	59.3	60.5	53.4	52.0
T1	51.0	53.4	53.3	53.3	58.8	59.3	52.1	55.0
T2	52.2	51.9	46.4	42.7	58.5	57.2	46.2	50.8
T3	53.8	54.4	53.3	54.1	58.3	58.2	50.6	54.4
T4	52.6	53.8	52.4	10.0	22.3	65.5	59.3	55.7
T5	53.7	54.1	53.7	54.3	62.9	60.1	52.9	55.7
T6	52.6	50.0	47.9	7.1	9.5	62.0	61.3	54.8
T7	52.7	51.0	55.1	57.3	60.1	59.7	52.5	54.7
T8	53.1	54.7	54.7	54.8	61.1	60.8	44.3	56.9
T9	55.2	54.8	54.5	53.8	60.9	60.0	56.1	57.2

SAMPLE	JULY		AUGUST		JUL-AUG	
	AVERAGE	Std. Dev.	AVERAGE	Std. Dev.	AVERAGE	Std. Dev.
	CH4 %	CH4 %	CH4 %	CH4 %	CH4 %	CH4 %
M0	52.1	0.880	52.5	3.144	52.2	2.057
M1	54.0	2.375	56.2	2.237	54.8	2.563
M2	53.6	2.307	56.1	4.337	54.6	3.435
M3	52.9	1.362	53.3	2.361	53.0	1.813
M4	49.6	1.483	51.4	2.238	50.3	2.006
M5	53.7	2.838	53.1	3.057	53.5	2.933
M6	52.4	2.157	52.1	4.337	52.3	3.159
M7	54.5	2.421	55.6	2.504	54.9	2.509
M8	55.3	3.302	54.3	3.138	54.9	3.278
M9	54.5	2.296	57.8	5.852	55.8	4.322
T0	55.9	1.786	55.3	3.721	55.7	2.694
T1	54.0	2.574	55.5	2.958	54.5	2.819
T2	50.3	5.409	51.4	4.511	50.7	5.117
T3	54.8	1.791	54.4	3.103	54.6	2.377
T4	38.2	18.438	60.2	4.047	46.4	18.208
T5	55.7	3.588	56.2	2.963	55.9	3.376
T6	33.4	20.574	59.4	3.242	43.1	20.648
T7	55.2	3.242	55.6	3.013	55.4	3.164
T8	55.7	2.782	54.0	7.041	55.0	4.908
T9	55.8	2.571	57.8	1.642	56.6	2.452

AVERAGE DAILY METHANE PRODUCTION PER REACTOR @ STP

SAMPLE	29/6-4/7	5/7-11/7	12/7-18/7	19/7-25/7	26/7-1/8	2/8-8/8	9/8-15/8	16/8-22/8	23/8-25/8
	CH4	CH4	CH4	CH4	CH4	CH4	CH4	CH4	CH4
	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)	AVERAGE (L/day)
M0	0.386	0.956	0.752	0.617	1.010	0.928	0.825	1.261	1.040
M1	0.731	0.952	0.733	0.378	0.882	0.863	0.777	0.763	0.738
M2	0.915	1.159	0.401	0.385	0.147	0.043	0.000	0.195	0.862
M3	0.675	0.639	0.619	0.636	0.341	0.763	0.589	0.637	0.647
M4	0.686	0.571	0.795	0.631	0.372	0.125	0.043	0.078	0.946
M5	0.790	0.893	0.978	0.817	1.116	0.836	0.537	0.793	0.741
M6	0.751	0.661	0.686	0.626	0.791	0.953	0.754	0.872	0.600
M7	0.913	0.960	1.153	1.442	1.460	1.388	1.358	1.424	1.269
M8	0.847	0.879	0.942	0.889	0.942	0.692	0.568	0.840	0.736
M9	0.613	1.016	0.880	1.011	0.836	0.667	0.485	1.179	0.945
T0	1.350	1.207	1.088	1.289	1.730	1.558	0.887	0.845	0.672
T1	1.003	1.351	1.222	0.648	1.340	1.195	1.154	1.155	1.033
T2	0.717	0.637	0.156	0.135	0.267	0.042	0.034	0.010	0.024
T3	0.706	0.738	0.543	0.444	0.567	0.451	0.379	0.637	0.517
T4	0.981	0.820	0.518	0.034	0.230	0.985	0.597	0.987	0.394
T5	1.213	1.540	1.343	1.296	1.775	1.817	1.631	1.751	1.429
T6	1.145	0.521	0.559	0.029	0.139	1.281	1.022	1.409	1.221
T7	1.010	0.724	0.691	0.684	0.999	0.795	0.720	0.934	1.017
T8	0.904	0.800	0.650	0.555	0.679	0.659	0.431	1.245	1.326
T9	0.937	1.249	0.947	0.954	0.973	0.857	1.028	0.892	1.012

SAMPLE	JULY	JULY	AUGUST	AUGUST	JUL-AUG	JUL-AUG
	CH4	CH4	CH4	CH4	CH4	CH4
	AVERAGE (L/day)	Std. Dev. (L/day)	AVERAGE (L/day)	Std. Dev. (L/day)	AVERAGE (L/day)	Std. Dev. (L/day)
M0	0.846	0.145	1.014	0.162	0.921	0.174
M1	0.735	0.198	0.785	0.047	0.757	0.153
M2	0.581	0.350	0.080	0.073	0.359	0.363
M3	0.682	0.082	0.659	0.064	0.672	0.075
M4	0.593	0.120	0.073	0.033	0.362	0.274
M5	0.919	0.118	0.727	0.114	0.833	0.151
M6	0.703	0.060	0.795	0.133	0.744	0.109
M7	1.166	0.257	1.360	0.058	1.252	0.218
M8	0.900	0.037	0.709	0.098	0.815	0.118
M9	0.911	0.086	0.819	0.265	0.870	0.193
T0	1.335	0.217	0.991	0.338	1.182	0.326
T1	1.113	0.264	1.134	0.061	1.123	0.201
T2	0.382	0.246	0.028	0.012	0.225	0.255
T3	0.600	0.108	0.511	0.118	0.560	0.121
T4	0.516	0.353	0.891	0.170	0.683	0.341
T5	1.433	0.202	1.657	0.148	1.533	0.211
T6	0.479	0.392	1.233	0.140	0.814	0.485
T7	0.821	0.150	0.866	0.116	0.841	0.138
T8	0.718	0.122	0.915	0.380	0.805	0.287
T9	1.012	0.119	0.947	0.074	0.983	0.106

AVERAGE DAILY BIOGAS PRODUCTION PER UNIT MASS @ STP

SAMPLE	28/6-4/7	5/7-11/7	12/7-18/7	19/7-25/7	25/7-1/8	2/8-8/8	9/8-15/8	16/8-22/8	23/8-25/8
	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)
M0	1.930	2.030	1.603	1.339	2.110	1.831	1.887	2.663	2.198
M1	2.770	3.594	2.808	1.417	3.004	2.915	2.889	2.738	2.550
M2	3.027	4.172	1.452	1.419	0.596	0.144	0.000	0.673	0.283
M3	3.253	3.023	3.024	2.990	3.810	3.383	2.905	3.024	3.070
M4	3.543	2.814	3.751	3.202	1.877	0.584	0.221	0.371	0.221
M5	3.198	3.376	3.636	3.030	3.827	2.911	2.132	3.075	2.870
M6	2.937	2.550	2.653	2.473	2.796	3.529	3.272	3.104	2.134
M7	3.115	3.627	4.245	5.362	4.942	4.771	5.205	5.060	4.508
M8	3.209	3.283	3.503	3.268	3.047	2.370	2.237	3.135	2.748
M9	2.543	3.142	2.763	3.162	2.358	1.903	1.603	3.037	2.433
T0	2.782	2.408	2.186	2.619	3.241	2.862	1.846	1.806	1.436
T1	3.332	5.060	4.587	2.431	4.560	4.031	4.431	4.199	3.757
T2	3.437	3.069	0.838	0.788	1.139	0.184	0.184	0.050	0.117
T3	3.277	3.390	2.546	2.054	2.431	1.939	1.873	3.204	2.377
T4	3.727	3.050	1.976	0.676	2.065	3.007	2.014	3.545	3.570
T5	4.519	5.693	5.000	4.772	5.644	6.046	6.167	6.287	5.130
T6	4.357	2.083	2.335	0.824	2.934	4.133	3.334	5.144	4.457
T7	3.834	2.839	2.508	2.387	3.323	2.662	2.743	3.416	3.719
T8	3.404	2.929	2.377	2.024	2.221	2.169	1.945	4.377	4.661
T9	2.830	3.798	2.895	2.957	2.662	2.380	3.055	2.600	2.948

SAMPLE	JULY	JULY	AUGUST	AUGUST	JUL-AUG	JUL-AUG
	AVERAGE (L/kg*day)	Std. Dev. (L/kg*day)	AVERAGE (L/kg*day)	Std. Dev. (L/kg*day)	AVERAGE (L/kg*day)	Std. Dev. (L/kg*day)
M0	1.802	0.289	2.145	0.330	1.955	0.352
M1	2.719	0.714	2.798	0.109	2.754	0.539
M2	2.133	1.288	0.275	0.251	1.307	1.342
M3	3.220	0.310	3.095	0.177	3.165	0.266
M4	2.997	0.635	0.349	0.149	1.820	1.402
M5	3.413	0.288	2.747	0.363	3.117	0.463
M6	2.682	0.167	3.010	0.528	2.827	0.407
M7	4.258	0.824	4.886	0.268	4.537	0.711
M8	3.262	0.147	2.623	0.350	2.978	0.409
M9	2.794	0.319	2.244	0.546	2.549	0.513
T0	2.647	0.358	1.987	0.530	2.354	0.551
T1	4.114	0.914	4.104	0.246	4.110	0.701
T2	1.854	1.154	0.134	0.056	1.090	1.213
T3	2.740	0.513	2.348	0.531	2.566	0.556
T4	2.299	1.039	3.034	0.630	2.626	0.954
T5	5.126	0.469	5.907	0.457	5.473	0.605
T6	2.507	1.153	4.267	0.651	3.289	1.301
T7	2.978	0.537	3.135	0.446	3.048	0.505
T8	2.591	0.506	3.288	1.238	2.901	0.971
T9	3.028	0.397	2.746	0.270	2.903	0.374

AVERAGE DAILY METHANE PRODUCTION PER UNIT MASS @ STP

SAMPLE	28/6-4/7	5/7-11/7	12/7-18/7	19/7-25/7	26/7-1/8	2/8-8/8	9/8-15/8	16/8-22/8	23/8-25/8
	CH4	CH4	CH4	CH4	CH4	CH4	CH4	CH4	CH4
	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)	AVERAGE (L/kg*day)
M0	0.384	1.074	0.835	0.686	1.123	1.031	0.817	1.401	1.156
M1	1.483	1.905	1.466	0.755	1.764	1.725	1.554	1.525	1.476
M2	1.630	2.318	0.803	0.771	0.293	0.086	0.000	0.391	0.164
M3	1.688	1.598	1.548	1.591	2.103	1.908	1.473	1.594	1.618
M4	1.715	1.428	1.763	1.578	0.931	0.812	0.107	0.194	0.116
M5	1.580	1.785	1.956	1.633	2.231	1.671	1.075	1.587	1.481
M6	1.502	1.322	1.372	1.251	1.582	1.906	1.508	1.744	1.199
M7	1.627	1.920	2.305	2.385	2.921	2.777	2.717	2.849	2.538
M8	1.695	1.759	1.885	1.778	1.883	1.384	1.137	1.651	1.473
M9	1.356	1.693	1.467	1.685	1.394	1.112	0.808	1.955	1.574
T0	1.511	1.341	1.209	1.433	1.922	1.732	0.986	0.939	0.746
T1	2.007	2.703	2.445	1.296	2.681	2.391	2.308	2.309	2.066
T2	1.793	1.593	0.389	0.336	0.667	0.105	0.085	0.026	0.060
T3	1.765	1.845	1.357	1.111	1.418	1.128	0.948	1.743	1.293
T4	1.962	1.640	1.035	0.068	0.461	1.970	1.194	1.974	1.988
T5	2.426	3.081	2.685	2.591	3.550	3.634	3.262	3.502	2.857
T6	2.291	1.042	1.118	0.059	0.279	2.562	2.043	2.819	2.442
T7	2.020	1.448	1.382	1.368	1.997	1.589	1.440	1.869	2.034
T8	1.808	1.601	1.300	1.109	1.357	1.318	0.862	2.490	2.652
T9	1.582	2.081	1.578	1.591	1.621	1.428	1.714	1.487	1.686

SAMPLE	JULY		AUGUST		JUL-AUG	
	CH4	CH4	CH4	CH4	CH4	CH4
	AVERAGE (L/kg*day)	Std. Dev. (L/kg*day)	AVERAGE (L/kg*day)	Std. Dev. (L/kg*day)	AVERAGE (L/kg*day)	Std. Dev. (L/kg*day)
M0	0.940	0.161	1.126	0.180	1.023	0.193
M1	1.470	0.397	1.570	0.094	1.515	0.306
M2	1.163	0.720	0.160	0.145	0.717	0.739
M3	1.706	0.204	1.648	0.160	1.680	0.188
M4	1.483	0.300	0.182	0.082	0.905	0.686
M5	1.837	0.237	1.453	0.229	1.667	0.301
M6	1.406	0.120	1.589	0.266	1.487	0.219
M7	2.332	0.514	2.720	0.115	2.504	0.436
M8	1.800	0.074	1.418	0.195	1.630	0.236
M9	1.519	0.144	1.365	0.441	1.450	0.322
T0	1.483	0.241	1.101	0.375	1.313	0.362
T1	2.226	0.528	2.269	0.122	2.245	0.403
T2	0.956	0.616	0.069	0.030	0.562	0.637
T3	1.499	0.271	1.278	0.295	1.401	0.303
T4	1.033	0.706	1.782	0.339	1.366	0.683
T5	2.867	0.404	3.314	0.295	3.065	0.423
T6	0.958	0.785	2.467	0.280	1.628	0.969
T7	1.643	0.300	1.733	0.232	1.683	0.276
T8	1.435	0.244	1.831	0.760	1.611	0.573
T9	1.687	0.198	1.579	0.123	1.639	0.177

AVERAGE DAILY BIOGAS PRODUCTION PER UNIT MASS as TS @ STP

SAMPLE	28/6-4/7	5/7-11/7	12/7-18/7	19/7-25/7	26/7-1/8	2/8-8/8	9/8-15/8	16/8-22/8	23/8-25/8
	AVERAGE	AVERAGE	AVERAGE	AVERAGE	AVERAGE	AVERAGE	AVERAGE	AVERAGE	AVERAGE
	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)
M0	7.005	7.368	5.820	4.860	7.659	6.647	6.848	9.667	7.977
M1	11.102	14.403	11.254	5.679	12.042	11.682	11.580	10.974	10.520
M2	12.836	17.691	6.155	6.018	2.528	0.609	0.000	2.855	1.201
M3	8.321	7.732	7.736	7.649	9.747	3.654	7.430	7.736	7.653
M4	9.024	7.596	10.124	6.641	5.066	1.576	0.596	1.000	0.596
M5	11.310	11.938	12.857	10.714	13.533	10.295	7.540	10.875	10.150
M6	8.660	7.521	7.824	7.293	8.242	10.407	9.648	9.154	6.292
M7	9.542	11.112	13.004	16.426	15.138	14.614	15.943	15.500	13.809
M8	11.273	11.532	12.308	11.480	10.705	8.326	7.860	11.015	9.653
M9	13.507	15.684	14.675	16.791	12.524	10.108	8.515	16.127	12.923
T0	10.136	8.772	7.962	9.541	11.807	10.427	6.723	6.578	5.230
T1	13.719	17.655	15.004	8.484	15.909	14.066	15.460	14.651	13.108
T2	9.121	8.145	2.223	2.090	3.024	0.489	0.489	0.133	0.311
T3	8.911	9.218	6.924	5.584	6.612	5.271	5.093	8.711	6.463
T4	13.463	11.018	7.137	2.441	7.460	10.863	7.275	12.803	12.894
T5	14.286	17.999	15.809	15.088	17.843	19.115	19.496	13.878	16.219
T6	13.735	6.567	7.361	2.598	9.251	13.029	10.509	16.217	14.051
T7	15.038	11.137	9.837	9.362	13.035	10.443	10.758	13.399	14.586
T8	14.641	12.596	10.222	8.705	9.553	9.327	8.366	18.824	20.049
T9	14.633	19.640	14.969	15.288	13.762	12.306	15.796	13.444	15.245

SAMPLE	JULY	JULY	AUGUST	AUGUST	JUL-AUG	JUL-AUG
	AVERAGE	AVERAGE	AVERAGE	AVERAGE	AVERAGE	AVERAGE
	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)	(L/kgTS*d)
M0	6.542	1.048	7.785	1.199	7.095	1.277
M1	10.896	2.864	11.214	0.437	11.037	2.160
M2	9.046	5.461	1.166	1.064	5.544	5.692
M3	8.237	0.792	7.919	0.452	8.096	0.682
M4	8.090	1.715	0.942	0.401	4.913	3.784
M5	12.070	1.019	9.715	1.285	11.024	1.637
M6	7.908	0.493	8.875	1.557	8.338	1.201
M7	13.044	2.523	14.967	0.822	13.899	2.179
M8	11.460	0.516	9.213	1.231	10.461	1.437
M9	14.836	1.695	11.918	2.897	13.539	2.726
T0	9.643	1.306	7.239	1.930	8.575	2.007
T1	14.354	3.191	14.321	0.858	14.340	2.446
T2	4.921	3.063	0.356	0.147	2.892	3.220
T3	7.450	1.394	6.385	1.443	6.976	1.512
T4	8.304	3.753	10.959	2.276	9.484	3.445
T5	16.205	1.482	18.677	1.445	17.304	1.912
T6	7.902	3.635	13.452	2.052	10.369	4.101
T7	11.682	2.106	12.296	1.751	11.955	1.980
T8	11.144	2.176	14.142	5.323	12.476	4.177
T9	15.658	2.055	14.198	1.396	15.009	1.934

AVERAGE DAILY METHANE PRODUCTION PER UNIT MASS as TS @ STP

SAMPLE	28/6-4/7	5/7-11/7	12/7-18/7	19/7-25/7	26/7-1/8	2/8-8/8	9/8-15/8	16/8-22/8	23/8-25/8
	CH4	CH4	CH4	CH4	CH4	CH4	CH4	CH4	CH4
	AVERAGE (L/kgTS*d)	AVERAGE (L/kgTS*d)	AVERAGE (L/kgTS*d)	AVERAGE (L/kgTS*d)	AVERAGE (L/kgTS*d)	AVERAGE (L/kgTS*d)	AVERAGE (L/kgTS*d)	AVERAGE (L/kgTS*d)	AVERAGE (L/kgTS*d)
M0	3.573	3.898	3.032	2.488	4.074	3.742	3.328	5.085	4.196
M1	5.863	7.635	5.875	3.027	7.069	6.916	6.230	6.112	5.915
M2	6.912	9.828	3.404	3.268	1.244	0.366	0.000	1.656	0.697
M3	4.319	4.087	3.961	4.069	5.380	4.881	3.767	4.077	4.139
M4	4.628	3.855	4.758	4.260	2.513	0.843	0.288	0.524	0.312
M5	5.588	6.312	6.917	5.775	7.890	5.909	3.800	5.611	5.237
M6	4.428	3.900	4.045	3.690	4.565	5.620	4.448	5.144	3.536
M7	4.983	5.883	7.061	8.837	8.946	8.506	8.322	8.727	7.775
M8	5.953	6.178	6.621	5.245	6.515	4.362	3.993	5.904	5.174
M9	7.199	8.993	7.793	8.949	7.402	5.903	4.291	10.424	8.361
T0	5.504	4.886	4.403	5.219	7.002	6.308	3.590	3.420	2.719
T1	7.002	9.430	8.530	4.522	9.354	8.341	8.054	8.058	7.209
T2	4.759	4.227	1.032	0.892	1.763	0.280	0.226	0.068	0.158
T3	4.798	5.017	3.691	3.021	3.855	3.068	2.577	4.739	3.516
T4	7.086	5.922	3.740	0.244	1.664	7.115	4.314	7.132	7.182
T5	7.669	9.740	8.489	8.193	11.223	11.488	10.313	11.072	9.034
T6	7.222	3.284	3.526	0.184	0.879	8.078	6.442	8.887	7.700
T7	7.923	5.678	5.420	5.364	7.834	6.234	5.648	7.329	7.978
T8	7.779	5.884	5.592	4.771	5.837	5.671	3.706	10.711	11.408
T9	8.077	10.763	8.158	8.225	8.381	7.384	8.862	7.690	8.720

SAMPLE	JULY	JULY	AUGUST	AUGUST	JUL-AUG	JUL-AUG
	CH4	CH4	CH4	CH4	CH4	CH4
	AVERAGE (L/kgTS*d)	Std. Dev. (L/kgTS*d)	AVERAGE (L/kgTS*d)	Std. Dev. (L/kgTS*d)	AVERAGE (L/kgTS*d)	Std. Dev. (L/kgTS*d)
M0	3.413	0.583	4.088	0.652	3.713	0.700
M1	5.894	1.590	6.293	0.376	6.071	1.227
M2	4.931	3.053	0.680	0.615	3.042	3.132
M3	4.363	0.522	4.216	0.409	4.298	0.481
M4	4.003	0.809	0.492	0.223	2.442	1.852
M5	6.496	0.836	5.140	0.809	5.893	1.065
M6	4.146	0.354	4.687	0.784	4.386	0.645
M7	7.142	1.574	8.332	0.352	7.671	1.335
M8	6.323	0.260	4.983	0.685	5.727	0.830
M9	8.067	0.762	7.247	2.342	7.703	1.711
T0	5.403	0.880	4.010	1.367	4.783	1.319
T1	7.768	1.843	7.916	0.424	7.833	1.404
T2	2.536	1.634	0.183	0.079	1.490	1.689
T3	4.076	0.737	3.475	0.902	3.809	0.823
T4	3.731	2.549	6.436	1.225	4.933	2.466
T5	9.063	1.277	10.477	0.933	9.691	1.337
T6	3.019	2.474	7.777	0.882	5.134	3.055
T7	6.444	1.177	6.797	0.911	6.601	1.081
T8	6.172	1.049	7.874	3.270	6.929	2.465
T9	8.721	1.026	8.164	0.638	8.473	0.918

AVERAGE DAILY BIOGAS PRODUCTION PER UNIT VOLUME @ STP

SAMPLE	28/6-4/7	5/7-11/7	12/7-18/7	19/7-25/7	26/7-1/8	2/8-8/8	9/8-15/8	16/8-22/8	23/8-25/8
	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)
M0	0.826	0.869	0.686	0.573	0.903	0.784	0.807	1.140	0.941
M1	1.291	1.675	1.308	0.650	1.400	1.358	1.346	1.276	1.235
M2	1.473	2.030	0.706	0.691	0.290	0.070	0.000	0.328	0.138
M3	0.836	0.777	0.777	0.768	0.979	0.869	0.746	0.777	0.789
M4	0.960	0.808	1.077	0.919	0.539	0.168	0.063	0.106	0.063
M5	1.334	1.408	1.516	1.263	1.596	1.214	0.889	1.282	1.197
M6	0.981	0.852	0.886	0.828	0.933	1.178	1.092	1.036	0.712
M7	1.098	1.279	1.497	1.891	1.742	1.682	1.835	1.784	1.590
M8	1.329	1.359	1.450	1.353	1.261	0.981	0.926	1.298	1.138
M9	1.417	1.750	1.539	1.761	1.314	1.060	0.893	1.691	1.355
T0	1.194	1.033	0.938	1.124	1.390	1.228	0.792	0.775	0.616
T1	1.618	2.082	1.887	1.001	1.876	1.659	1.823	1.728	1.546
T2	0.956	0.853	0.233	0.219	0.317	0.051	0.051	0.014	0.033
T3	0.954	0.986	0.741	0.596	0.708	0.564	0.545	0.932	0.692
T4	1.588	1.299	0.842	0.288	0.880	1.281	0.858	1.510	1.521
T5	1.663	2.095	1.840	1.756	2.077	2.225	2.269	2.314	1.888
T6	1.596	0.763	0.855	0.302	1.075	1.514	1.221	1.884	1.633
T7	1.757	1.302	1.150	1.094	1.523	1.220	1.257	1.566	1.705
T8	1.673	1.440	1.168	0.995	1.092	1.066	0.956	2.152	2.292
T9	1.554	2.085	1.589	1.623	1.461	1.307	1.677	1.427	1.619

SAMPLE	JULY	JULY	AUGUST	AUGUST	JUL-AUG	JUL-AUG
	AVERAGE (L/L*day)	Std. Dev. (L/L*day)	AVERAGE (L/L*day)	Std. Dev. (L/L*day)	AVERAGE (L/L*day)	Std. Dev. (L/L*day)
M0	0.771	0.124	0.918	0.141	0.837	0.151
M1	1.267	0.333	1.304	0.051	1.283	0.251
M2	1.038	0.627	0.134	0.122	0.636	0.653
M3	0.828	0.080	0.796	0.045	0.813	0.068
M4	0.860	0.182	0.100	0.043	0.522	0.402
M5	1.423	0.120	1.146	0.152	1.300	0.193
M6	0.895	0.056	1.005	0.176	0.944	0.136
M7	1.501	0.290	1.723	0.095	1.600	0.251
M8	1.350	0.061	1.086	0.145	1.233	0.169
M9	1.556	0.178	1.250	0.304	1.420	0.286
T0	1.136	0.154	0.853	0.227	1.010	0.236
T1	1.693	0.376	1.689	0.101	1.691	0.288
T2	0.515	0.321	0.037	0.015	0.303	0.337
T3	0.797	0.149	0.683	0.154	0.747	0.162
T4	0.979	0.443	1.292	0.268	1.118	0.406
T5	1.886	0.173	2.174	0.168	2.014	0.223
T6	0.918	0.422	1.563	0.238	1.205	0.476
T7	1.365	0.246	1.437	0.205	1.397	0.231
T8	1.274	0.249	1.616	0.608	1.426	0.477
T9	1.563	0.218	1.507	0.148	1.594	0.205

AVERAGE DAILY METHANE PRODUCTION PER UNIT VOLUME @ STP

SAMPLE	28/6-4/7	5/7-11/7	12/7-18/7	19/7-25/7	26/7-1/8	2/8-8/8	9/8-15/8	16/8-22/8	23/8-25/8
	CH4	CH4	CH4	CH4	CH4	CH4	CH4	CH4	CH4
	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)	AVERAGE (L/L*day)
M0	0.421	0.460	0.358	0.293	0.480	0.441	0.392	0.600	0.495
M1	0.682	0.888	0.683	0.352	0.822	0.804	0.724	0.711	0.688
M2	0.793	1.128	0.391	0.375	0.143	0.042	0.000	0.190	0.080
M3	0.434	0.411	0.398	0.409	0.541	0.490	0.378	0.410	0.416
M4	0.492	0.410	0.506	0.453	0.267	0.090	0.031	0.056	0.033
M5	0.659	0.744	0.816	0.681	0.930	0.697	0.448	0.662	0.618
M6	0.501	0.442	0.458	0.413	0.528	0.636	0.504	0.582	0.400
M7	0.574	0.677	0.813	1.017	1.030	0.979	0.958	1.004	0.895
M8	0.702	0.728	0.780	0.736	0.730	0.573	0.471	0.696	0.610
M9	0.755	0.943	0.817	0.939	0.776	0.619	0.450	1.094	0.877
T0	0.648	0.575	0.518	0.615	0.825	0.743	0.423	0.403	0.320
T1	0.826	1.112	1.006	0.533	1.103	0.984	0.950	0.950	0.850
T2	0.499	0.443	0.108	0.093	0.185	0.029	0.024	0.007	0.017
T3	0.514	0.537	0.395	0.323	0.412	0.328	0.276	0.507	0.376
T4	0.836	0.698	0.441	0.029	0.196	0.839	0.509	0.841	0.847
T5	0.893	1.134	0.988	0.954	1.306	1.337	1.200	1.289	1.052
T6	0.839	0.382	0.410	0.021	0.102	0.939	0.749	1.033	0.895
T7	0.926	0.664	0.633	0.627	0.916	0.729	0.660	0.857	0.932
T8	0.889	0.797	0.539	0.545	0.667	0.648	0.424	1.224	1.304
T9	0.858	1.143	0.866	0.873	0.890	0.784	0.941	0.816	0.926

SAMPLE	JULY	JULY	AUGUST	AUGUST	JUL-AUG	JUL-AUG
	CH4	CH4	CH4	CH4	CH4	CH4
	AVERAGE (L/L*day)	Std. Dev. (L/L*day)	AVERAGE (L/L*day)	Std. Dev. (L/L*day)	AVERAGE (L/L*day)	Std. Dev. (L/L*day)
M0	0.402	0.069	0.482	0.077	0.438	0.083
M1	0.685	0.185	0.732	0.044	0.706	0.143
M2	0.566	0.350	0.078	0.071	0.349	0.359
M3	0.438	0.052	0.424	0.041	0.432	0.048
M4	0.426	0.086	0.052	0.024	0.260	0.197
M5	0.766	0.099	0.606	0.095	0.695	0.126
M6	0.469	0.040	0.531	0.089	0.497	0.073
M7	0.822	0.181	0.959	0.041	0.883	0.154
M8	0.745	0.031	0.587	0.081	0.675	0.098
M9	0.846	0.080	0.760	0.246	0.808	0.179
T0	0.636	0.104	0.472	0.161	0.563	0.155
T1	0.916	0.217	0.934	0.050	0.924	0.166
T2	0.266	0.171	0.019	0.008	0.156	0.177
T3	0.436	0.079	0.372	0.086	0.408	0.088
T4	0.440	0.301	0.759	0.144	0.582	0.291
T5	1.055	0.149	1.219	0.109	1.128	0.156
T6	0.351	0.287	0.904	0.102	0.596	0.355
T7	0.753	0.138	0.794	0.106	0.771	0.126
T8	0.705	0.120	0.900	0.374	0.792	0.282
T9	0.926	0.109	0.867	0.068	0.900	0.097

B3: TOTAL SOLIDS VOLATILE SOLIDS and pH

Solids and pH Data

Tu 4/7/89

SAMPLE	TS (%)	VS (XTS)	VS (%)	pH
M0	21.11	93.13	23.88	8.85
M1	21.95	93.31	20.48	9.20
M2	20.02	94.34	18.92	9.10
M3	37.50	94.12	35.33	8.00
M4	37.74	95.81	36.16	7.40
M5	30.10	93.95	28.27	8.50
M6	37.12	93.53	34.72	8.20
M7	32.97	94.46	31.14	8.35
M8	30.18	94.83	28.62	8.75
M9	17.05	93.62	15.97	9.30
T0	24.58	94.59	23.26	9.10
T1	27.10	93.21	25.26	9.20
T2	38.27	94.97	36.34	8.15
T3	35.59	95.36	34.04	8.75
T4	26.68	95.69	25.53	8.60
T5	32.09	95.33	30.59	9.00
T6	31.63	96.03	30.43	8.55
T7	27.09	93.31	25.28	8.80
T8	23.60	94.64	22.34	9.00
T9	19.55	94.62	18.59	9.20

Fri 7/7/89

M0	25.82	95.47	24.65	8.60
M1	22.39	93.06	20.84	9.00
M2	21.17	94.81	20.07	8.50
M3	38.18	94.34	36.01	7.70
M4	38.67	95.97	37.11	7.00
M5	28.39	94.06	26.71	8.50
M6	35.23	94.41	33.26	7.50
M7	32.87	94.49	31.06	8.20
M8	30.21	94.60	28.58	8.70
M9	17.23	93.75	16.15	9.00
T0	24.69	94.57	23.35	9.00
T1	27.22	93.19	25.37	9.00
T2	37.22	94.37	35.12	8.00
T3	36.84	96.06	35.39	8.60
T4	27.09	95.88	25.98	8.25
T5	32.30	93.87	30.32	8.90
T6	32.56	96.46	31.41	8.20
T7	26.15	93.87	24.54	8.80
T8	23.30	94.68	22.06	8.95
T9	19.07	94.49	18.02	9.05

Solids and pH Data

Tues 11/7/89

SAMPLE	TS (%)	VS (XTS)	VS (%)	pH
M0	27.60	95.59	26.38	8.50
M1	28.67	95.35	27.33	8.80
M2	23.58	95.33	22.48	9.00
M3	38.25	94.78	36.25	7.70
M4	38.99	96.44	37.61	6.00
M5	28.09	94.20	26.46	8.50
M6	34.26	94.26	32.29	7.60
M7	31.51	95.09	29.96	8.50
M8	29.78	95.27	28.37	8.60
M9	19.23	94.19	18.11	9.00
T0	27.83	94.64	26.34	9.00
T1	31.06	93.23	28.96	9.20
T2	37.63	95.05	35.76	7.50
T3	36.27	96.19	34.89	8.80
T4	28.83	96.07	27.69	7.90
T5	31.48	94.22	29.66	8.90
T6	33.55	96.46	32.36	7.50
T7	25.71	94.07	24.19	9.00
T8	24.13	95.06	22.93	9.00
T9	18.44	94.70	17.46	9.00

Fri 14/7/89

M0	27.51	95.44	26.25	7.30
M1	26.70	94.43	25.21	8.60
M2	22.83	95.65	21.84	8.50
M3	38.18	93.93	35.86	7.50
M4	37.92	96.08	36.43	6.05
M5	27.43	93.91	25.76	8.60
M6	33.83	94.53	31.98	7.40
M7	30.35	95.73	29.05	8.50
M8	28.06	95.10	26.69	8.60
M9	18.80	94.80	17.82	8.40
T0	28.71	95.06	27.29	9.00
T1	29.00	93.06	26.99	9.10
T2	38.53	94.35	36.45	7.30
T3	36.75	96.56	35.48	8.60
T4	26.95	96.11	25.90	7.90
T5	31.42	94.30	29.63	8.90
T6	33.33	96.80	32.27	7.10
T7	26.68	94.38	25.18	9.00
T8	24.62	95.07	23.40	9.00
T9	18.68	95.45	17.83	9.00

Solids and pH Data

Tues 18/7/89

SAMPLE	TS (%)	VS (%TS)	VS (%)	pH
M0	27.45	96.15	26.39	6.90
M1	25.81	93.86	24.23	8.60
M2	23.00	95.40	21.94	6.60
M3	39.10	93.85	36.69	7.50
M4				
M5	27.71	93.65	25.95	8.50
M6	34.85	93.68	32.64	7.50
M7	31.61	95.04	30.04	8.50
M8	28.25	94.89	26.81	8.70
M9	17.79	94.52	16.82	8.80
T0	27.92	94.83	26.47	9.10
T1	28.77	92.62	26.65	7.00
T2	39.67	93.60	37.21	8.40
T3	34.13	96.05	32.34	8.40
T4	28.48	96.02	27.34	7.40
T5	32.10	93.70	30.08	8.80
T6	32.60	96.05	31.31	6.70
T7	26.11	93.38	24.38	8.90
T8	23.40	94.84	22.19	8.90
T9	18.47	94.84	17.52	8.30

Fri 21/7/89

M0	28.09	96.39	27.07	
M1	26.03	94.21	24.52	
M2	23.64	96.21	22.74	
M3	38.80	94.49	36.66	
M4	36.46	94.94	34.62	
M5	27.78	94.04	26.12	
M6	33.00	94.26	31.11	
M7	31.45	95.68	30.09	
M8	28.62	95.78	27.42	
M9	18.19	95.32	17.34	
T0	28.64	96.01	27.50	
T1	29.12	93.11	27.11	
T2	36.54	93.80	34.28	
T3	37.09	96.58	35.83	
T4	28.63	96.43	27.61	
T5	32.93	94.14	31.00	
T6	33.22	96.54	32.07	
T7	26.51	93.75	24.85	
T8	23.58	96.20	22.69	
T9	18.51	96.17	17.80	

Tue 25/7/89

SAMPLE	TS (%)	VS (%TS)	VS (%)	pH
M0	28.47	96.56	27.49	
M1	26.30	94.62	24.89	
M2	23.33	96.35	22.48	
M3	37.96	94.43	35.85	
M4	36.54	95.16	34.77	
M5	28.24	94.10	26.57	
M6	33.75	94.35	31.84	
M7	32.57	95.60	31.14	
M8	27.80	95.74	26.62	
M9	17.95	95.54	17.17	
T0	28.67	95.65	27.48	
T1	29.11	93.10	27.10	
T2	36.33	94.74	34.42	
T3	38.17	95.36	36.63	
T4	30.22	96.65	29.21	
T5	31.72	93.79	29.75	
T6	32.23	98.28	31.67	
T7	27.41	94.13	25.80	
T8	23.67	96.07	22.74	
T9	18.71	95.80	17.92	

Fri 28/7/89

M0	29.22	95.80	27.99	9.05
M1	26.46	94.12	24.91	8.50
M2	23.55	96.39	22.70	7.55
M3	40.36	94.36	38.08	8.70
M4	39.44	94.78	37.38	7.30
M5	28.88	93.92	27.12	7.40
M6	34.39	93.65	32.21	7.30
M7	29.97	96.17	28.82	8.30
M8	28.38	96.11	27.28	8.00
M9	18.08	95.82	17.33	7.70
T0	28.79	94.93	27.33	8.70
T1	28.69	93.42	26.80	8.75
T2	38.91	94.22	36.66	8.50
T3	36.57	95.83	35.05	8.30
T4	30.09	95.33	28.83	6.40
T5	33.47	93.84	31.41	8.70
T6	35.18	95.92	33.74	6.10
T7	26.90	93.67	25.20	8.70
T8	23.58	95.76	22.58	8.65
T9	18.58	96.09	17.86	8.00

JULY 1989
AVERAGE

SAMPLE	TS (%)	VS (%TS)	VS (%)	pH
M0	26.91	98.07	26.26	8.20
M1	25.54	94.12	24.05	8.78
M2	22.64	95.59	21.65	8.54
M3	38.54	94.30	36.34	7.87
M4	37.97	95.60	36.30	6.75
M5	28.33	93.98	26.62	8.35
M6	34.55	94.08	32.50	7.58
M7	31.66	95.28	30.16	8.39
M8	28.91	95.29	27.55	8.56
M9	18.04	94.69	17.09	8.70
T0	27.48	95.06	26.13	8.98
T1	28.76	93.12	26.78	8.71
T2	37.90	94.41	35.78	7.98
T3	36.45	96.07	35.02	8.58
T4	28.37	96.09	27.26	7.74
T5	32.19	94.15	30.31	8.87
T6	33.05	96.57	31.91	7.36
T7	26.57	93.82	24.93	8.87
T8	23.73	95.29	22.62	8.92
T9	18.76	95.27	17.88	8.84

JULY 1989
Std. Dev.

SAMPLE	TS (%)	VS (%TS)	VS (%)	pH
M0	2.374	5.706	1.296	3.619
M1	2.112	0.681	2.147	3.809
M2	1.245	0.654	1.309	3.724
M3	0.826	0.282	0.781	3.424
M4	1.076	0.590	1.119	3.092
M5	0.789	0.155	0.746	3.635
M6	1.163	0.370	1.018	3.293
M7	1.041	0.574	0.853	3.635
M8	0.921	0.499	0.801	3.712
M9	0.680	0.768	0.699	3.794
T0	1.676	0.529	1.682	3.892
T1	1.159	0.213	1.080	3.831
T2	1.098	0.448	1.007	3.474
T3	1.082	0.369	1.081	3.716
T4	1.283	0.297	1.278	3.407
T5	0.665	0.491	0.614	3.840
T6	0.991	0.707	0.905	3.268
T7	0.527	0.347	0.502	3.841
T8	0.403	0.587	0.404	3.863
T9	0.384	0.646	0.325	3.844

JULY 1989

AVERAGE FEED VALUES

SAMPLE	TS (%)	VS (XTS)	VS (%)	pH
F 2-20	20.46	96.42	19.73	4.69
F 2-25	24.36	96.90	23.60	5.28
F 2-30	30.49	97.20	29.63	4.63
F 2-35	33.92	97.23	32.98	4.63
F 2-40	38.81	97.23	37.73	4.64
F 1-25	25.23	94.67	24.63	5.38
F 1-30	29.74	94.75	28.18	5.53
F 1-35	34.53	94.84	32.75	5.21
F 1-40	39.96	95.06	37.99	5.18

JULY 1989

AVERAGE

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA AI/AP	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
F 2-20	0.00	0.00	0.62	0.62	*	0.00	0.00	2.93	2.93
F 2-25	0.00	0.00	0.37	0.37	*	0.00	0.00	1.48	1.48
F 2-30	0.00	0.00	0.49	0.49	*	0.00	0.00	1.50	1.50
F 2-35	0.00	0.00	0.62	0.62	*	0.00	0.00	1.81	1.81
F 2-40	0.00	0.00	0.58	0.58	*	0.00	0.00	1.49	1.49
F 1-25	0.00	0.00	0.80	0.80	*	0.00	0.00	2.87	2.87
F 1-30	0.00	0.00	0.64	0.64	*	0.00	0.00	2.12	2.12
F 1-35	0.00	0.00	0.73	0.73	*	0.00	0.00	2.10	2.10
F 1-40	0.00	0.00	0.72	0.72	*	0.00	0.00	1.80	1.80

* does not exist

Solids and pH Data

Wed 2/8/89

SAMPLE	TS (%)	VS (%TS)	VS (%)	pH
M0	28.05	95.81	26.87	8.70
M1	24.79	93.88	23.27	8.56
M2	23.05	96.85	22.32	6.10
M3	38.90	94.49	36.75	7.75
M4	37.90	93.48	35.43	9.40
M5	28.28	93.73	26.51	7.85
M6	33.30	94.06	31.33	5.60
M7	32.11	96.10	30.86	7.90
M8	27.82	96.07	26.73	8.20
M9	17.53	35.77	16.79	8.17
T0	25.95	95.92	24.89	8.80
T1	27.45	93.54	25.68	8.90
T2	37.43	94.71	35.45	7.75
T3	37.06	35.66	35.45	8.10
T4				
T5	31.52	92.97	29.30	9.20
T6				
T7	24.57	93.55	22.99	8.40
T8	22.50	96.13	21.63	8.35
T9	24.05	97.14	23.37	7.55

Mon 7/8/89

M0	30.75	96.28	29.61	6.10
M1	25.77	93.99	24.23	8.75
M2	26.63	94.92	25.34	9.25
M3	40.94	95.19	38.98	8.00
M4	41.12	94.44	38.84	9.05
M5	29.33	94.21	27.63	7.00
M6	35.48	92.59	32.86	9.70
M7	33.63	96.09	32.31	7.55
M8	28.78	96.47	27.77	7.80
M9	18.51	96.05	17.78	7.25
T0	27.12	96.23	26.10	8.75
T1	30.02	93.16	27.97	8.95
T2	40.94	95.08	38.93	6.05
T3	38.39	95.71	36.75	7.85
T4				
T5	32.42	93.38	30.27	9.25
T6				
T7	25.12	93.87	23.58	8.50
T8	23.62	96.32	22.75	8.45
T9	18.13	96.36	17.47	8.05

Solids and pH Data

Fri 11/8/89

SAMPLE	TS (%)	VS (%TS)	VS (%)	pH
M0	28.43	96.31	27.38	5.50
M1	25.11	93.49	23.48	8.90
M2				
M3	40.04	94.26	37.75	7.80
M4				
M5	28.82	94.21	27.15	6.70
M6	34.04	92.35	31.44	9.15
M7	40.10	96.89	38.85	7.80
M8	29.00	96.15	27.89	6.85
M9	20.13	96.33	19.54	6.40
T0	28.09	96.44	27.09	8.50
T1	29.47	93.28	27.49	8.20
T2	29.78	94.59	27.63	8.50
T3	37.86	96.46	36.52	7.20
T4	27.31	94.24	25.74	9.60
T5	31.86	93.15	29.70	9.00
T6	31.34	94.55	29.63	9.70
T7	25.15	93.54	23.52	8.30
T8	22.91	96.06	22.00	8.30
T9	18.96	96.25	18.25	8.50

Wed 15/8/89

M0	28.40	95.44	27.11	8.90
M1	24.39	94.12	22.95	8.50
M2	25.78	94.27	24.30	9.30
M3	40.13	94.53	37.93	6.70
M4	36.02	95.02	34.23	7.30
M5				6.70
M6	32.92	92.99	30.62	6.70
M7	32.12	96.07	30.86	8.50
M8	27.97	96.27	26.93	7.80
M9	20.29	96.55	19.59	7.00
T0	27.92	96.05	26.82	7.30
T1	28.96	93.26	27.01	8.50
T2	36.12	93.89	33.91	9.40
T3	55.38	30.10	19.68	8.50
T4	27.22	94.51	25.72	9.40
T5	32.69	92.80	30.33	9.00
T6	31.12	94.67	29.46	9.40
T7	24.74	93.64	23.17	8.00
T8	23.36	96.10	22.45	8.20
T9	19.70	96.26	18.97	8.20

Solids and pH Data

Mon 21/8/89

SAMPLE	TS (%)	VS (VTS)	VS (%)	pH
M0	25.82	94.31	24.35	9.00
M1	24.69	93.35	23.05	8.35
M2	23.66	93.70	22.17	9.30
M3	40.66	93.53	38.03	7.05
M4	33.49	94.90	31.78	7.10
M5	27.77	92.62	25.72	9.05
M6	32.46	91.94	29.84	6.70
M7	32.02	95.57	30.60	8.75
M8	26.54	95.25	25.66	9.05
M9	20.72	94.95	19.68	8.00
T0	27.49	95.98	26.38	7.60
T1	28.44	92.77	26.39	8.40
T2	36.32	92.67	33.66	9.30
T3	35.27	94.97	33.49	9.20
T4	26.07	95.21	24.82	9.35
T5	27.21	92.08	25.06	8.90
T6	29.57	94.85	28.42	9.20
T7	22.89	93.14	21.32	8.00
T8	22.10	95.82	21.18	7.95
T9	19.01	95.01	18.25	8.85

Fri 25/8/89

M0	27.69	94.79	26.25	8.60
M1	21.42	93.66	20.06	8.00
M2	23.49	94.43	22.18	9.30
M3	37.19	93.60	34.81	6.90
M4	32.12	95.54	30.69	6.00
M5	26.95	93.27	25.14	8.50
M6	31.40	93.36	29.32	6.60
M7	31.80	95.82	30.47	8.90
M8	27.61	95.47	26.36	9.20
M9	20.47	95.62	19.58	8.35
T0	27.85	96.11	26.77	7.65
T1	27.01	92.83	25.08	8.10
T2	34.22	94.46	32.32	8.80
T3	36.67	95.58	35.05	8.86
T4	27.38	95.65	26.19	8.90
T5	30.72	93.05	28.59	8.45
T6	29.15	95.39	27.80	9.00
T7	24.04	93.35	22.44	8.55
T8	22.13	96.08	21.26	8.20
T9	19.66	96.20	18.91	8.30

AUGUST,89
AVERAGE

Solids and pH Data

SAMPLE	TS (%)	VS (%TS)	VS (%)	pH
M0	28.19	95.49	26.93	7.80
M1	24.36	93.75	22.84	8.51
M2	24.53	94.83	23.26	8.65
M3	39.64	94.27	37.37	7.37
M4	36.13	94.68	34.19	7.77
M5	28.23	93.61	26.43	7.63
M6	33.27	92.88	30.90	7.41
M7	33.63	96.09	32.32	8.23
M8	28.02	95.95	26.89	8.15
M9	19.62	95.96	18.83	7.53
T0	27.41	96.12	26.34	8.10
T1	28.56	93.14	26.60	8.51
T2	37.47	94.23	35.32	8.30
T3	37.05	95.68	35.45	8.24
T4	27.00	94.90	25.62	9.31
T5	31.07	92.91	28.88	8.97
T6	30.39	94.86	28.83	9.33
T7	24.42	93.52	22.84	8.29
T8	22.77	96.08	21.88	8.24
T9	19.92	96.37	19.20	8.24

AUGUST,89
Std. Dev.

Solids and pH Data

SAMPLE	TS (%)	VS (%TS)	VS (%)	pH
M0	1.448	0.737	1.557	1.431
M1	1.386	0.273	1.311	0.288
M2	1.433	1.082	1.314	1.275
M3	1.272	0.573	1.318	0.500
M4	3.197	0.692	2.871	1.273
M5	0.826	0.605	0.911	0.884
M6	1.275	0.692	1.154	1.484
M7	2.955	0.407	2.982	0.508
M8	0.699	0.437	0.773	0.801
M9	1.177	0.619	1.128	0.700
T0	0.723	0.174	0.722	0.601
T1	1.063	0.267	1.005	0.322
T2	2.278	0.785	2.313	1.145
T3	10.606	24.445	5.974	0.660
T4	0.535	0.558	0.496	0.256
T5	1.840	0.409	1.808	0.261
T6	0.889	0.323	0.752	0.259
T7	0.778	0.228	0.776	0.221
T8	0.580	0.146	0.583	0.157
T9	1.923	0.360	1.928	0.399

B4: ALKALINITY

Alkalinity Data

Tues 11/7

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0	0.00	0.29	0.53	0.24	0.83	0.00	1.04	1.91	0.87
M1	0.00	0.35	0.75	0.40	1.14	0.00	1.22	2.61	1.39
M2	0.05	0.44	0.78	0.34	0.78	0.21	1.87	3.33	1.45
M3									
M4	0.00	0.10	0.89	0.79	8.00	0.00	0.25	2.29	2.04
M5	0.00	0.23	0.47	0.23	1.00	0.00	0.83	1.55	0.83
M6	0.00	0.20	0.60	0.40	2.00	0.00	0.58	1.74	1.16
M7	0.00	0.20	0.54	0.34	1.75	0.00	0.62	1.70	1.08
M8	0.00	0.19	0.78	0.58	3.00	0.00	0.65	2.61	1.96
M9									
T0	0.14	0.65	1.02	0.37	0.57	0.50	2.34	3.67	1.34
T1	0.10	0.64	0.38	0.34	0.54	0.32	2.05	3.16	1.10
T2	0.00	0.20	1.23	1.03	5.25	0.00	0.52	3.27	2.75
T3	0.00	0.35	0.65	0.30	0.86	0.00	0.96	1.79	0.83
T4	0.00	0.15	0.87	0.73	5.00	0.00	0.51	3.03	2.53
T5	0.00	0.34	0.82	0.48	1.43	0.00	1.08	2.62	1.54
T6	0.00	0.21	1.09	0.88	4.25	0.00	0.62	3.25	2.63
T7	0.05	0.45	0.80	0.35	0.78	0.20	1.76	3.13	1.37
T8	0.00	0.30	0.50	0.20	0.67	0.00	1.24	2.07	0.83
T9	0.10	0.84	1.04	0.20	0.24	0.54	4.57	5.65	1.08

Fri 14/7/

M0
M1
M2
M3
M4
M5
M6
M7
M8
M9

T0
T1
T2
T3
T4
T5
T6
T7
T8
T9

Alkalinity Data

Tu 4/7/89

SAMPLE	ALKAL. PHENDLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA	ALKAL. PHENDLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0	0.05	0.45	0.84	0.40	0.89	0.23	2.11	3.99	1.88
M1	0.05	0.51	1.01	0.40	0.67	0.23	2.76	4.60	1.84
M2	0.05	0.39	0.58	0.19	0.50	0.24	1.95	2.92	0.97
M3	0.00	0.21	0.54	0.32	1.50	0.00	0.57	1.43	0.86
M4	0.00	0.16	0.63	0.47	3.00	0.00	0.41	1.66	1.24
M5	0.00	0.15	0.44	0.29	2.00	0.00	0.49	1.46	0.98
M6	0.00	0.21	0.70	0.48	2.25	0.00	0.58	1.88	1.30
M7	0.00	0.15	0.53	0.39	2.67	0.00	0.44	1.62	1.18
M8	0.00	0.96	1.52	0.56	0.58	0.00	3.19	5.04	1.85
M9	0.08	0.75	1.05	0.30	0.40	0.44	4.40	5.16	1.76
T0	0.14	0.66	1.14	0.47	0.71	0.58	2.70	4.63	1.93
T1	0.05	0.53	0.86	0.33	0.64	0.18	1.94	3.17	1.23
T2	0.00	0.55	1.21	0.65	1.18	0.00	1.45	3.15	1.71
T3	0.00	0.29	0.87	0.58	2.00	0.00	0.81	2.43	1.62
T4	0.00	0.78	1.55	0.78	1.00	0.00	2.91	5.83	2.91
T5	0.00	0.25	0.54	0.30	1.20	0.00	0.77	1.69	0.92
T6	0.00	0.15	0.59	0.44	3.00	0.00	0.47	1.87	1.40
T7	0.05	0.64	0.74	0.10	0.15	0.18	2.37	2.73	0.36
T8									
T9	0.23	0.88	1.30	0.42	0.47	1.18	4.50	6.53	2.13

Fri 7/7/8

- M0
- M1
- M2
- M3
- M4
- M5
- M6
- M7
- M8
- M9

- T0
- T1
- T2
- T3
- T4
- T5
- T6
- T7
- T8
- T9

Tues 18/77

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0	0.00	0.20	0.82	0.62	3.13	0.00	0.72	2.99	2.26
M1	0.00	0.44	1.03	0.59	1.33	0.00	1.71	3.99	2.28
M2	0.00	0.36	0.87	0.51	1.40	0.00	1.58	3.78	2.21
M3	0.00	0.17	0.77	0.50	3.57	0.00	0.43	1.98	1.55
M4									
M5	0.00	0.37	0.89	0.53	1.44	0.00	1.32	3.21	1.89
M6	0.00	0.20	1.16	0.96	4.75	0.00	0.58	3.34	2.76
M7	0.00	0.33	0.95	0.62	1.86	0.00	1.05	3.01	1.96
M8	0.00	0.46	1.02	0.56	1.22	0.00	1.63	3.63	1.99
M9	0.02	0.88	1.42	0.53	0.61	0.13	4.96	7.96	3.00
T0	0.03	1.02	1.42	0.40	0.39	0.10	3.66	5.10	1.44
T1	0.08	0.86	1.54	0.68	0.79	0.27	3.00	5.37	2.37
T2	0.00	0.44	3.22	2.78	6.33	0.00	1.11	8.12	7.02
T3	0.00	0.40	1.46	1.05	2.63	0.00	1.17	4.26	3.08
T4	0.00	0.22	2.03	1.81	8.22	0.00	0.77	7.13	6.36
T5	0.00	0.50	1.41	0.80	1.33	0.00	1.88	4.39	2.51
T6	0.00	0.35	3.11	2.77	8.00	0.00	1.06	9.54	8.48
T7	0.00	0.86	1.51	0.65	0.75	0.00	3.29	5.77	2.47
T8	0.00	0.87	1.55	0.67	0.77	0.00	3.73	6.60	2.88
T9	0.17	1.28	1.81	0.52	0.41	0.90	6.95	9.79	2.83

Fri 21/77

M0
M1
M2
M3
M4
M5
M6
M7
M8
M9

T0
T1
T2
T3
T4
T5
T6
T7
T8
T9

Tue 25/77

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0									
M1									
M2									
M3									
M4									
M5									
M6									
M7									
M8									
M9									
T0									
T1									
T2									
T3									
T4									
T5									
T6									
T7									
T8									
T9									

Fri 28/77

M0	0.08	0.98	3.13	2.15	2.20	0.27	3.34	10.70	7.35
M1	0.00	0.15	0.84	0.70	4.75	0.00	0.55	3.19	2.63
M2	0.00	0.15	0.84	0.69	4.50	0.00	0.65	3.57	2.92
M3	0.00	0.35	1.47	1.13	3.22	0.00	0.87	3.65	2.79
M4	0.00	0.67	4.90	4.24	6.35	0.00	1.69	12.43	10.74
M5	0.00	0.20	0.71	0.51	2.60	0.00	0.68	2.46	1.78
M6	0.00	0.28	2.10	1.82	6.57	0.00	0.81	5.11	5.30
M7	0.00	0.27	0.73	0.46	1.71	0.00	0.89	2.42	1.53
M8	0.00	0.27	0.68	0.42	1.57	0.00	0.94	2.41	1.47
M9	0.00	0.65	1.23	0.57	0.88	0.00	3.62	6.79	3.17
T0	0.15	0.73	1.25	0.51	0.70	0.51	2.55	4.34	1.79
T1	0.24	1.45	1.77	0.32	0.22	0.84	5.06	6.18	1.12
T2	0.08	0.74	2.44	1.71	2.32	0.20	1.89	6.28	4.39
T3	0.00	0.35	0.92	0.58	1.67	0.00	0.95	2.52	1.58
T4	0.00	0.94	7.42	6.48	6.32	0.00	3.12	24.67	21.55
T5	0.00	0.82	1.61	0.78	0.95	0.00	2.46	4.80	2.34
T6	0.00	0.42	5.71	5.29	12.62	0.00	1.19	16.23	15.04
T7	0.04	0.60	1.20	0.60	1.00	0.15	2.22	4.44	2.22
T8	0.07	0.95	1.41	0.46	0.48	0.30	4.05	6.00	1.95
T9	0.00	0.99	1.42	0.43	0.43	0.00	5.32	7.62	2.30

JULY 1989
AVERAGE

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA AI/AP	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0	0.03	0.48	1.33	0.85	1.78	0.13	1.81	4.90	3.09
M1	0.01	0.39	0.91	0.52	1.35	0.06	1.56	3.60	2.04
M2	0.02	0.34	0.77	0.43	1.29	0.11	1.51	3.40	1.89
M3	0.00	0.24	0.93	0.68	2.80	0.00	0.62	2.35	1.73
M4	0.00	0.31	2.14	1.83	5.96	0.00	0.79	5.46	4.67
M5	0.00	0.24	0.63	0.39	1.66	0.00	0.83	2.20	1.37
M6	0.00	0.22	1.14	0.92	4.10	0.00	0.64	3.27	2.63
M7	0.00	0.24	0.69	0.45	1.92	0.00	0.75	2.19	1.44
M8	0.00	0.47	1.00	0.53	1.13	0.00	1.60	3.42	1.82
M9	0.02	0.57	0.92	0.35	0.62	0.14	3.24	5.23	1.98
T0	0.11	0.77	1.21	0.44	0.57	0.42	2.81	4.44	1.62
T1	0.12	0.87	1.29	0.42	0.48	0.40	3.01	4.47	1.46
T2	0.02	0.48	2.03	1.54	3.21	0.05	1.24	5.21	3.97
T3	0.00	0.35	0.97	0.63	1.81	0.00	0.97	2.75	1.78
T4	0.00	0.52	2.97	2.45	4.71	0.00	1.83	10.16	8.34
T5	0.00	0.50	1.10	0.59	1.18	0.00	1.55	3.38	1.83
T6	0.00	0.28	2.63	2.35	8.37	0.00	0.83	7.72	6.89
T7	0.03	0.64	1.06	0.42	0.66	0.13	2.41	4.02	1.61
T8	0.02	0.53	0.86	0.33	0.63	0.07	2.25	3.67	1.41
T9	0.12	1.00	1.39	0.39	0.39	0.66	5.34	7.42	2.09

JULY 1989
Std. Dev.

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA AI/AP	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0	0.033	0.301	1.044	0.761	0.958	0.126	1.025	3.428	2.513
M1	0.022	0.166	0.117	0.127	1.521	0.100	0.805	0.759	0.466
M2	0.024	0.110	0.111	0.184	1.596	0.114	0.516	0.320	0.741
M3	0.000	0.125	0.530	0.413	0.905	0.000	0.312	1.308	1.020
M4	0.000	0.255	1.956	1.704	2.080	0.000	0.643	4.935	4.301
M5	0.000	0.081	0.185	0.130	0.601	0.000	0.307	0.694	0.471
M6	0.000	0.032	0.595	0.566	1.884	0.000	0.098	1.757	1.665
M7	0.000	0.071	0.172	0.105	0.390	0.000	0.237	0.568	0.343
M8	0.000	0.300	0.324	0.065	0.887	0.000	0.983	1.041	0.206
M9	0.031	0.340	0.549	0.228	0.195	0.180	1.932	3.085	1.267
	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
T0	0.050	0.150	0.148	0.056	0.128	0.190	0.506	0.518	0.242
T1	0.074	0.357	0.380	0.151	0.207	0.259	1.250	1.336	0.527
T2	0.034	0.196	0.853	0.808	2.096	0.086	0.500	2.098	2.003
T3	0.000	0.040	0.296	0.271	0.638	0.000	0.130	0.914	0.817
T4	0.000	0.343	2.603	2.369	2.726	0.000	1.194	8.504	7.774
T5	0.000	0.227	0.429	0.212	0.180	0.000	0.665	1.270	0.637
T6	0.000	0.108	2.014	1.910	3.746	0.000	0.300	5.699	5.412
T7	0.021	0.146	0.310	0.218	0.314	0.078	0.558	1.191	0.825
T8	0.031	0.397	0.642	0.255	0.120	0.130	1.696	2.742	1.092
T9	0.086	0.173	0.276	0.119	0.091	0.442	0.988	1.533	0.638

Alkalinity Data

Wed 2/8/8

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0	0.00	0.47	2.70	2.23	4.70	0.00	1.69	9.63	7.94
M1	0.00	0.25	0.53	0.44	1.80	0.00	0.99	2.77	1.78
M2	0.00	0.09	1.32	1.23	13.50	0.00	0.39	5.73	5.33
M3	0.00	0.29	1.78	1.49	5.08	0.00	0.75	4.59	3.83
M4	0.88	4.27	11.63	7.36	1.72	2.33	11.26	30.68	19.42
M5	0.00	0.20	0.55	0.35	1.75	0.00	0.71	1.94	1.23
M6	0.00	0.02	2.52	2.50	103.00	0.00	0.07	7.58	7.51
M7	0.00	0.23	0.68	0.45	2.00	0.00	0.70	2.11	1.41
M8	0.00	0.19	0.56	0.37	2.00	0.00	0.67	2.00	1.34
M9	0.00	0.20	0.67	0.47	2.38	0.00	1.12	3.79	2.67
T0	0.03	0.99	1.44	0.46	0.46	0.10	3.80	5.56	1.76
T1	0.15	1.02	2.51	1.58	1.55	0.56	3.73	9.50	5.77
T2	0.00	0.40	2.37	1.97	4.94	0.00	1.07	6.33	5.26
T3	0.00	0.30	1.00	0.70	2.33	0.00	0.81	2.69	1.89
T4									
T5	0.88	2.43	3.39	0.95	0.39	2.80	7.72	10.75	3.03
T6									
T7	0.02	0.44	0.85	0.41	0.94	0.10	1.79	3.47	1.69
T8	0.05	0.87	1.29	0.41	0.47	0.22	3.88	5.71	1.83
T9	0.00	0.92	1.30	0.37	0.41	0.00	3.84	5.40	1.56

Mon 7/8/8

M0	0.00	0.12	2.28	2.16	17.40	0.00	0.40	7.42	7.02
M1	0.00	0.26	0.71	0.45	1.73	0.00	1.01	2.76	1.75
M2	0.10	1.43	4.76	3.33	2.33	0.36	5.35	17.84	12.49
M3	0.00	0.21	1.40	1.19	5.56	0.00	0.52	3.43	2.90
M4	0.00	1.09	7.09	5.99	5.48	0.00	2.65	17.24	14.58
M5	0.00	0.09	0.81	0.71	7.50	0.00	0.32	2.75	2.42
M6	0.56	2.85	7.71	4.86	1.70	1.58	8.03	21.73	13.70
M7	0.00	0.10	0.47	0.37	3.75	0.00	0.29	1.40	1.10
M8	0.00	0.12	0.50	0.38	3.20	0.00	0.41	1.72	1.31
M9	0.00	0.22	0.72	0.50	2.33	0.00	1.16	3.87	2.71
T0	0.12	0.80	1.22	0.42	0.53	0.43	2.93	4.48	1.55
T1	0.14	0.80	1.34	0.54	0.68	0.47	2.66	4.45	1.80
T2	0.00	0.35	4.31	3.96	11.27	0.00	0.86	10.53	9.67
T3	0.00	0.28	1.34	1.06	3.83	0.00	0.72	3.49	2.77
T4									
T5	0.46	1.73	2.54	0.81	0.47	1.42	5.34	7.83	2.49
T6									
T7	0.05	0.54	0.92	0.38	0.70	0.19	2.16	3.67	1.50
T8	0.02	0.72	1.17	0.46	0.63	0.10	3.04	4.97	1.93
T9	0.00	0.77	1.20	0.43	0.56	0.00	4.23	6.60	2.38

Alkalinity Data

Fri 11/8/

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0	0.00	0.00	1.53	1.53		0.00	0.00	5.37	5.37
M1	0.04	0.37	0.56	0.19	0.50	0.15	1.48	2.23	0.74
M2									
M3	0.00	0.19	0.98	0.79	4.20	0.00	0.47	2.44	1.97
M4									
M5	0.00	0.11	0.88	0.76	5.67	0.00	0.40	3.05	2.65
M6	0.12	1.42	7.41	5.99	4.22	0.35	4.17	21.76	17.60
M7	0.00	0.30	0.83	0.53	1.75	0.00	0.75	2.06	1.31
M8	0.00	0.20	0.88	0.68	3.40	0.00	0.69	3.04	2.35
M9	0.00	0.23	1.10	0.87	3.83	0.00	1.12	5.43	4.31
T0	0.05	0.37	0.63	0.26	0.71	0.19	1.30	2.23	0.93
T1	0.00	0.37	0.70	0.33	0.89	0.00	1.25	2.37	1.11
T2	0.08	0.76	2.67	1.90	2.50	0.19	1.92	6.70	4.79
T3	0.00	0.19	1.19	1.00	5.20	0.00	0.51	3.15	2.64
T4	1.63	4.54	5.59	1.06	0.23	5.98	16.61	20.48	3.87
T5	0.35	1.04	5.00	3.95	3.81	1.12	3.26	15.70	12.43
T6	2.16	5.25	6.78	1.53	0.29	6.89	16.76	21.63	4.87
T7	0.00	0.25	0.41	0.15	0.64	0.00	0.99	1.63	0.63
T8	0.00	0.29	0.55	0.26	0.90	0.00	1.27	2.41	1.14
T9	0.05	0.62	0.91	0.29	0.46	0.25	3.27	4.78	1.51

Wed 16/8/

M0	0.14	1.10	4.86	3.76	3.42	0.51	3.87	17.11	13.24
M1	0.04	0.40	0.89	0.48	1.20	0.17	1.65	3.63	1.98
M2	0.52	2.62	6.07	3.45	1.31	2.01	10.17	23.54	13.37
M3	0.00	0.12	1.59	1.47	12.33	0.00	0.30	3.97	3.67
M4	0.00	0.39	5.55	5.16	13.25	0.00	1.08	15.40	14.32
M5	0.00	0.50	2.32	1.83	3.69				
M6	0.00	0.59	5.87	5.27	8.88	0.00	1.80	17.82	16.02
M7	0.08	0.78	1.06	0.27	0.35	0.24	2.44	3.30	0.85
M8	0.00	0.26	0.96	0.70	2.71	0.00	0.93	3.44	2.51
M9	0.00	0.22	1.08	0.86	3.92	0.00	1.08	5.30	4.22
T0	0.00	0.21	0.86	0.65	3.17	0.00	0.74	3.08	2.34
T1	0.04	0.50	1.00	0.50	1.00	0.12	1.72	3.44	1.72
T2	0.67	2.90	7.09	4.20	1.45	1.85	8.02	19.64	11.62
T3	0.07	0.76	2.14	1.38	1.82	0.11	1.16	3.28	2.12
T4	1.67	4.37	6.27	1.90	0.43	6.14	16.07	23.04	6.97
T5	0.27	1.20	1.85	0.65	0.54	0.84	3.67	5.66	1.99
T6	1.25	4.43	6.67	2.23	0.50	4.02	14.24	21.42	7.18
T7	0.00	0.31	0.62	0.31	1.00	0.00	1.26	2.52	1.26
T8	0.00	0.39	0.74	0.35	0.90	0.00	1.66	3.15	1.49
T9	0.00	0.55	0.99	0.44	0.80	0.00	2.78	5.01	2.22

Alkalinity Data

Mon 21/8/

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0	0.18	2.38	7.30	4.91	2.06	0.70	9.23	28.26	19.03
M1	0.07	0.75	0.99	0.23	0.31	0.29	3.05	3.99	0.94
M2	0.44	3.21	5.47	2.26	0.71	1.86	13.56	23.13	9.56
M3	0.00	0.35	2.56	2.21	6.38	0.00	0.85	6.29	5.44
M4	0.00	0.62	4.62	4.00	6.50	0.00	1.84	13.78	11.94
M5	0.13	1.75	3.91	2.15	1.23	0.48	6.32	14.08	7.75
M6	0.00	0.76	6.46	5.70	7.48	0.00	2.35	19.90	17.55
M7	0.07	0.83	1.29	0.56	0.68	0.21	2.58	4.34	1.76
M8	0.43	2.37	3.47	1.10	0.46	1.61	8.79	12.88	4.09
M9	0.00	1.91	3.54	1.63	0.86	0.00	9.22	17.10	7.88
T0	0.00	0.31	1.75	1.45	4.71	0.00	1.12	6.38	5.26
T1	0.04	0.00	0.98	0.98		0.15	0.00	3.43	3.43
T2	0.95	3.56	6.61	3.03	0.85	2.62	9.85	18.21	8.35
T3	0.59	1.99	3.40	1.41	0.71	1.66	5.64	9.63	3.98
T4	0.72	2.75	3.92	1.12	0.40	2.74	10.71	15.02	4.31
T5	0.12	1.13	1.79	0.56	0.59	0.43	4.14	6.57	2.43
T6	0.60	2.52	3.96	1.44	0.57	2.01	8.39	13.20	4.81
T7	0.00	0.21	0.52	0.30	1.43	0.00	0.93	2.25	1.32
T8	0.00	0.27	0.92	0.65	2.44	0.00	1.21	4.17	2.96
T9	0.13	0.93	1.17	0.24	0.26	0.70	4.89	6.17	1.28

Fri 25/8/

M0	0.03	0.97	5.53	4.57	4.73	0.12	3.49	19.98	16.49
M1	0.00	0.43	0.67	0.23	0.54	0.00	2.02	3.11	1.09
M2	0.63	2.78	4.55	1.77	0.64	2.69	11.83	19.35	7.53
M3	0.00	0.20	1.82	1.62	8.25	0.00	0.53	4.88	4.35
M4	0.00	0.14	3.16	3.02	21.67	0.00	0.43	9.84	9.40
M5	0.02	0.78	3.00	2.22	2.83	0.08	2.90	11.13	8.23
M6	0.00	0.39	4.78	4.39	11.13	0.00	1.26	15.23	13.98
M7	0.09	0.88	1.70	0.83	0.95	0.30	2.75	5.35	2.60
M8	0.45	1.91	3.33	1.42	0.74	1.62	6.90	12.05	5.14
M9	0.00	0.62	2.64	2.02	3.24	0.00	3.04	12.89	9.85
T0	0.00	0.22	1.78	1.56	7.20	0.00	0.78	6.38	5.60
T1	0.00	0.40	0.82	0.42	1.05	0.00	1.47	3.02	1.55
T2	0.35	2.38	4.63	2.25	0.94	1.03	6.96	13.54	6.58
T3	0.43	2.01	3.90	1.89	0.94	1.17	5.47	10.62	5.15
T4	0.30	1.92	4.05	2.13	1.11	1.09	7.00	14.78	7.78
T5	0.02	0.81	1.56	0.75	0.92	0.07	2.64	5.07	2.43
T6	0.55	2.37	3.94	1.57	0.66	1.89	8.14	13.52	5.38
T7	0.04	0.74	1.31	0.57	0.77	0.18	3.08	5.46	2.38
T8	0.00	0.55	1.18	0.64	1.17	0.00	2.47	5.34	2.88
T9	0.00	0.62	1.07	0.45	0.73	0.00	3.13	5.43	2.30

AUGUST, 89
AVERAGE

Alkalinity Data

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA AI/AP	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0	0.06	0.84	4.03	3.19	3.79	0.22	3.11	14.63	11.51
M1	0.02	0.41	0.75	0.34	0.82	0.10	1.70	3.08	1.38
M2	0.34	2.03	4.43	2.41	1.19	1.38	8.26	17.92	9.65
M3	0.00	0.23	1.69	1.46	6.46	0.00	0.57	4.27	3.70
M4	0.18	1.30	6.41	5.11	3.92	0.47	3.46	17.39	13.93
M5	0.03	0.59	1.83	1.24	2.10	0.11	2.13	5.59	4.46
M6	0.11	1.01	5.79	4.78	4.75	0.32	2.95	17.34	14.39
M7	0.04	0.52	1.02	0.50	0.97	0.12	1.59	3.09	1.51
M8	0.15	0.84	1.62	0.78	0.92	0.54	3.06	5.85	2.79
M9	0.00	0.57	1.62	1.06	1.87	0.00	2.79	8.07	5.27
T0	0.03	0.48	1.28	0.80	1.67	0.12	1.78	4.69	2.91
T1	0.06	0.51	1.24	0.72	1.41	0.22	1.80	4.37	2.56
T2	0.34	1.73	4.61	2.89	1.67	0.95	4.78	12.49	7.71
T3	0.20	0.95	2.16	1.21	1.27	0.57	2.63	5.92	3.29
T4	1.08	3.40	4.96	1.55	0.46	3.99	12.60	18.33	5.73
T5	0.35	1.39	2.69	1.30	0.93	1.11	4.46	8.59	4.13
T6	1.14	3.64	5.34	1.69	0.46	3.70	11.88	17.44	5.56
T7	0.02	0.42	0.77	0.36	0.86	0.08	1.70	3.17	1.46
T8	0.01	0.51	0.98	0.46	0.90	0.05	2.25	4.29	2.04
T9	0.03	0.73	1.11	0.37	0.51	0.16	3.69	5.57	1.88

AUGUST, 89
Std. Dev.

Alkalinity Data

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA AI/AP	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
M0	0.074	0.798	2.030	1.288	5.556	0.280	3.089	7.994	5.083
M1	0.027	0.168	0.143	0.122	0.598	0.110	0.702	0.587	0.472
M2	0.246	1.133	1.647	0.867	4.939	1.028	4.792	6.472	3.001
M3	0.000	0.074	0.479	0.431	2.708	0.000	0.184	1.204	1.087
M4	0.353	1.517	2.906	1.513	7.035	0.932	3.975	7.082	3.321
M5	0.052	0.636	1.363	0.786	2.588	0.185	2.301	5.013	2.929
M6	0.205	0.925	1.753	1.148	36.026	0.577	2.587	4.922	3.439
M7	0.041	0.317	0.420	0.174	1.128	0.127	1.019	1.391	0.563
M8	0.207	0.928	1.271	0.378	1.140	0.760	3.429	4.714	1.401
M9	0.000	0.620	1.083	0.575	1.055	0.000	2.957	5.087	2.681
T0	0.042	0.301	0.429	0.512	2.521	0.155	1.167	1.589	1.835
T1	0.062	0.326	0.643	0.436	0.289	0.219	1.161	2.377	1.607
T2	0.361	1.279	1.783	0.922	3.674	0.999	3.614	5.168	2.428
T3	0.237	0.783	1.118	0.376	1.592	0.671	2.252	3.308	1.136
T4	0.592	1.096	1.005	0.469	0.336	2.154	3.969	3.548	1.672
T5	0.278	0.543	1.202	1.197	1.215	0.873	1.677	3.670	3.725
T6	0.650	1.234	1.387	0.316	0.137	2.025	3.724	4.084	0.961
T7	0.020	0.184	0.300	0.125	0.264	0.082	0.755	1.240	0.523
T8	0.018	0.223	0.264	0.143	0.646	0.082	0.977	1.186	0.672
T9	0.049	0.151	0.133	0.080	0.186	0.259	0.715	0.635	0.436

JULY 1988
 AVERAGE
 FEED-SUBSTRATE

SAMPLE	TS (%)	VS (%TS)	VS (%)	pH
F 2-20	20.46	96.42	19.73	4.69
F 2-25	24.36	96.90	23.60	5.28
F 2-30	30.49	97.20	29.63	4.63
F 2-35	33.92	97.23	32.98	4.63
F 2-40	38.81	97.23	37.73	4.64
F 1-25	26.23	94.67	24.83	5.38
F 1-30	29.74	94.75	28.18	5.53
F 1-35	34.53	94.84	32.75	5.21
F 1-40	39.96	95.06	37.99	5.18

JULY 1988
 AVERAGE
 FEED-SUBSTRATE

SAMPLE	ALKAL. PHENOLPH. (mg/g MS)	ALKAL. PARTIAL (mg/g MS)	ALKAL. TOTAL (mg/g MS)	ALKAL. INTERM. (mg/g MS)	ALFA AI/AP	ALKAL. PHENOLPH. (mg/g TS)	ALKAL. PARTIAL (mg/g TS)	ALKAL. TOTAL (mg/g TS)	ALKAL. INTERM. (mg/g TS)
F 2-20	0.00	0.00	0.62	0.62	*	0.00	0.00	2.93	2.93
F 2-25	0.00	0.00	0.37	0.37	*	0.00	0.00	1.48	1.48
F 2-30	0.00	0.00	0.49	0.49	*	0.00	0.00	1.50	1.50
F 2-35	0.00	0.00	0.62	0.62	*	0.00	0.00	1.81	1.81
F 2-40	0.00	0.00	0.58	0.58	*	0.00	0.00	1.49	1.49
F 1-25	0.00	0.00	0.80	0.80	*	0.00	0.00	2.87	2.87
F 1-30	0.00	0.00	0.64	0.64	*	0.00	0.00	2.12	2.12
F 1-35	0.00	0.00	0.73	0.73	*	0.00	0.00	2.10	2.10
F 1-40	0.00	0.00	0.72	0.72	*	0.00	0.00	1.80	1.80

* does not exist